

EVOLVE

Investigations on Capillary Cooling of the first wall

Preliminary results

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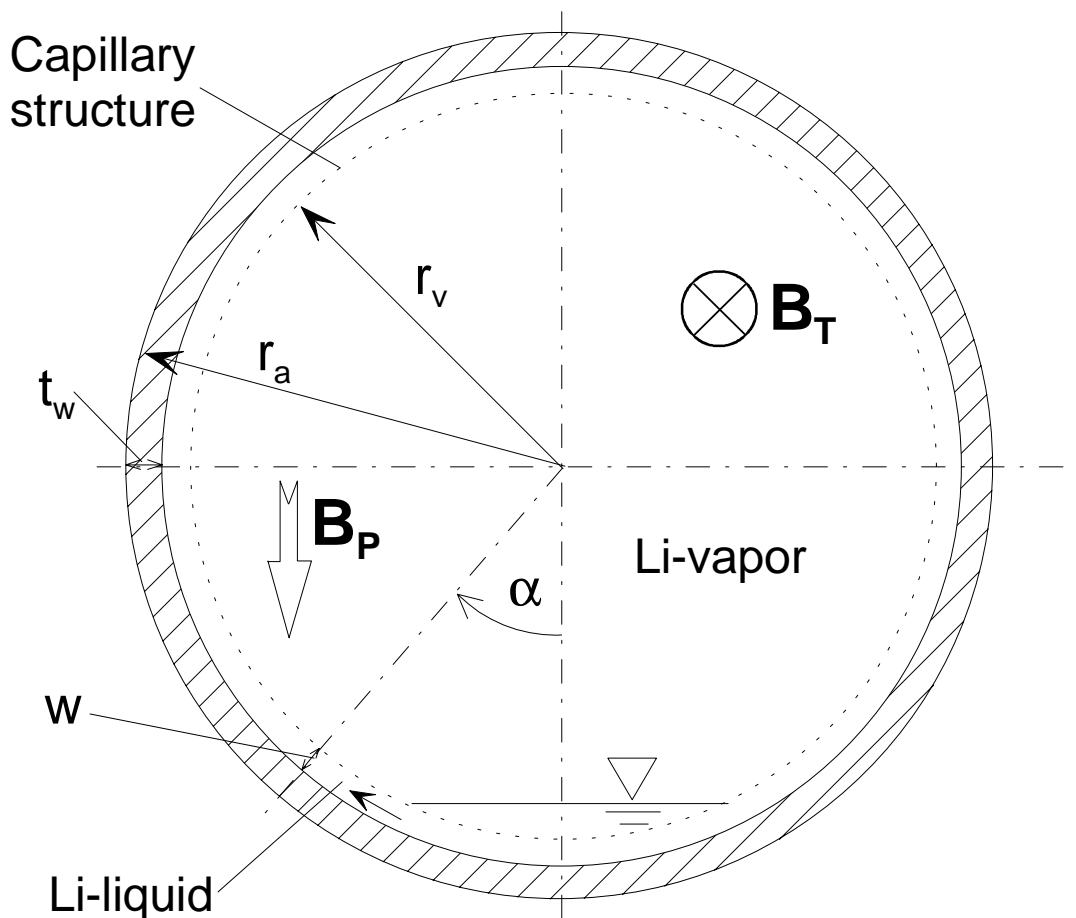
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EVOLVE–Concept: Capillary Cooling

The model:

- Feeding the liquid lithium through an azimuthal gap of the width w
- Evaporation and pumping of the liquid lithium in a capillary of the diameter d_c .



Simplifying assumptions and approximations:

- The toroidal field is exactly aligned with the tube (gap).
- The magnetic field perpendicular to the feeding gap $B_{\perp} = B_p \cdot \cos\alpha$ where $B_p = 1/10 B_T$.
- For pressure drop calculations $r_v = r_a$

- Δp_C = Capillary pressure head
 Δp_{H1} = Hydrostatic pressure head of the liquid
 Δp_{H2} = Pressure drop of the liquid in the feeding gap
 Δp_{H3} = Pressure drop of the liquid in the capillary
 Δp_{M1} = MHD pressure drop in the feeding gap due to the poloidal field
 Δp_{M2} = MHD pressure drop in the feeding gap due to the toroidal field
 Δp_{M3} = MHD pressure drop in the capillary due to the toroidal field

Limiting operation condition:

$$\Delta p_C > \Delta p_{H1} + \Delta p_{H2} + \Delta p_{H3} + \Delta p_{M1} + \Delta p_{M2} + \Delta p_{M3}$$

Chosen parameters:

Outer tube radius	$r_a = 0.03$	m
Tube length	$l_{ax} = 3.00$	m
Surface heat flux	$q''_0 = 2.0E+6$	W/m ²
Toroidal magnetic field strength	$B_T = 6.0$	Tesla
Thickness of the capillary structure	$t_c = 0.5E-3$	m
Area fraction of the capillaries	$\beta = 0.5$	

Thermophysical data of lithium [Vargaftik] and tungsten at 1200°C:

Lithium:

Density		
Liquid	$\rho_l = 411$	kg/m ³
Vapor	$\rho_v = 2.620E-2$	kg/m ³
Viscosity		
Liquid	$\mu_l = 0.169E-3$	Ns/m ²
Vapor	$\mu_v = 150E-7$	Ns/m ²

Heat conductivity		
Liquid	$\lambda_l = 62.1$	W/m K (T = 1300K)
Heat of vaporization	$h = 19.757E+6$	Ws/kg
Surface tension	$\sigma_c = 0.255$	N/m
Electrical conductivity	$\sigma_l = 3.03E+6$	A/Vm (T = 400°C)

Tungsten

Heat conductivity	$\lambda = 22.1$	W/m K (T=1400K estim.)
Electrical conductivity	$\sigma_l = 2.00E+6$	A/Vm (T = 1400°C)

Capillary pressure head:

$$\Delta p_C = 2\sigma_c/r_c = 1.02/d_c \quad \text{N/m}^2$$

Hydrostatic pressure:

$$\Rightarrow \Delta p_{H1} = \rho_l g 2r_v = 217.72 \quad \text{N/m}^2$$

Pressure drop of the liquid in the feeding gap:

$$\Delta p_{H2}(\alpha) = C_1/w^3(\alpha + \sin\alpha)$$

For full height ($\alpha = \Pi$) and

$$C_1 = (12\mu_l q''_0 r_a^2)/(\rho_l h) = 4.4955E+10$$

$$\Delta p_{H2}(\Pi) = 1.4123E-9 / w^3 \quad \text{N/m}^2$$

Pressure drop of the liquid in the capillary:

For $r_a \cong r_v$ and the length of the capillar $l_c \cong t_c$

$$\Rightarrow \Delta p_{H3} = (64 \mu_l q''_0 t_c) / (\Pi d_c^2 \rho_l h \beta) = 8.480E-10 / d_c^2$$

MHD pressure drop in the feeding gap due to the poloidal field:

$$\Delta p_{M1}(\alpha) = C_2 C_3(1/w) [(2r_a - r_v)((1/2)\alpha + (1/4) \sin 2\alpha) + r_v((1/12)\sin 3\alpha + (3/4)\sin\alpha)]$$

with $C_2 = C_w / (1 + C_w)$ as a first approximation where

$$C_w = (\sigma_w t_w) / (\sigma_l 0.5w) \quad \text{the corresponding wall conduction ratio}$$

$$C_w = (\sigma_w t_w) / (\sigma_l 0.5w) = 3.9604E-3/w$$

$$\Rightarrow C_2 = 3.9604E-3 / (w (1 + 3.9604E-3/w))$$

and $C_3 = (\sigma_l q''_0 r_v B_p^2) / (\rho_l h) = 7.254$

with $r_a \cong r_v$ and for full height ($\alpha = \Pi$)

$$\Delta p_{M1}(\Pi) = C_2 C_3 (1/w) r_a \Pi / 2 = 1.354E-3 / (w^2 (1 + 3.9604E-3/w))$$

MHD pressure drop in the feeding gap due to the toroidal field:

$$\Delta p_{M2}(\alpha) = C_4 C_5 (1/w) [2r_a \alpha + r_v (\sin \alpha - \alpha)]$$

with

where $C_{w,T} = (\sigma_{w,T} t_{w,T}) / (0.5 b_T \sigma_l)$ $t_{w,T} = 0.5E+3$ m choosen

$$C_{w,T} = 0.033$$

$$b_T = 20.0E+3$$
 m

$$\Rightarrow C_4 = 0.032$$

and $C_5 = (\sigma_l q''_0 r_v B_T^2) / (\rho_l h) = 725.4$

with $r_a \cong r_v$ and for full height ($\alpha = \Pi$):

$$\Rightarrow \Delta p_{M2}(\Pi) = C_4 C_5 (1/w) r_a \Pi = 2.321 / w$$

MHD pressure drop in the capillary due to the toroidal field:

$$\Delta p_{M3} = C_6 C_7$$

where $C_6 = C_{w3} / (1 + C_{w3})$

$$C_{w3} = (\sigma_w / \sigma_l) (t_w / r_c) = 0.66 = \text{const.}$$

$$C_7 = (\sigma_l q''_0 2r_a B_T^2 l_c) / (\Pi \beta r_v \rho_l h) = 19.00$$

With $l_c \cong t_c$

$$\Rightarrow \Delta p_{M3} = C_6 C_7 = 12.54 \quad \text{N/m}^2$$

Maximal superheating of the lithium at the wall:

$$T_{Li,w} = (q''_0 w_{eff}) / \lambda + T_s = 3.2206E+4 w_{eff} + 1473 \quad \text{K}$$

Where $w_{eff} \cong w + f t_c d$

$$F = f(\lambda_l / \lambda_w) < 1.0$$

Results:

Fig. 2 shows the dependance of the capillary pressure head from the capillary diameter d_C and the contributions of the different pressure drops to the total pressure drop of the liquid lithium needed to remove a heat flux of $q''_0 = 2.0E+6$ [W/m²] from the first wall for the choosen parameters given on page 3 and 5 in dependance of the gap width w . The calculations of the MHD pressure drop are conducted neglecting three-dimensional effects which may happen due to the changing magnetic field size and/or mass flow through within the feeding gap along the flow direction.

As can be seen from Fig. 2 the MHD pressure drop in the feeding gap caused by the toroidal field represents a considerable contribution to the total pressure drop which can only be reduced by reducing the thickness $t_{w,T}$ of wall connecting the capillary structure with the first wall and by increasing the toroidal distance b_T of thes walls.

Fig. 3 shows the capillary pressure head and the total pressure drop as a function of the capillary diameter d_C and of the gap width w respectively. In the figure the dependance of the minimal needed gap width w from the capillary diameter is shown on an example.

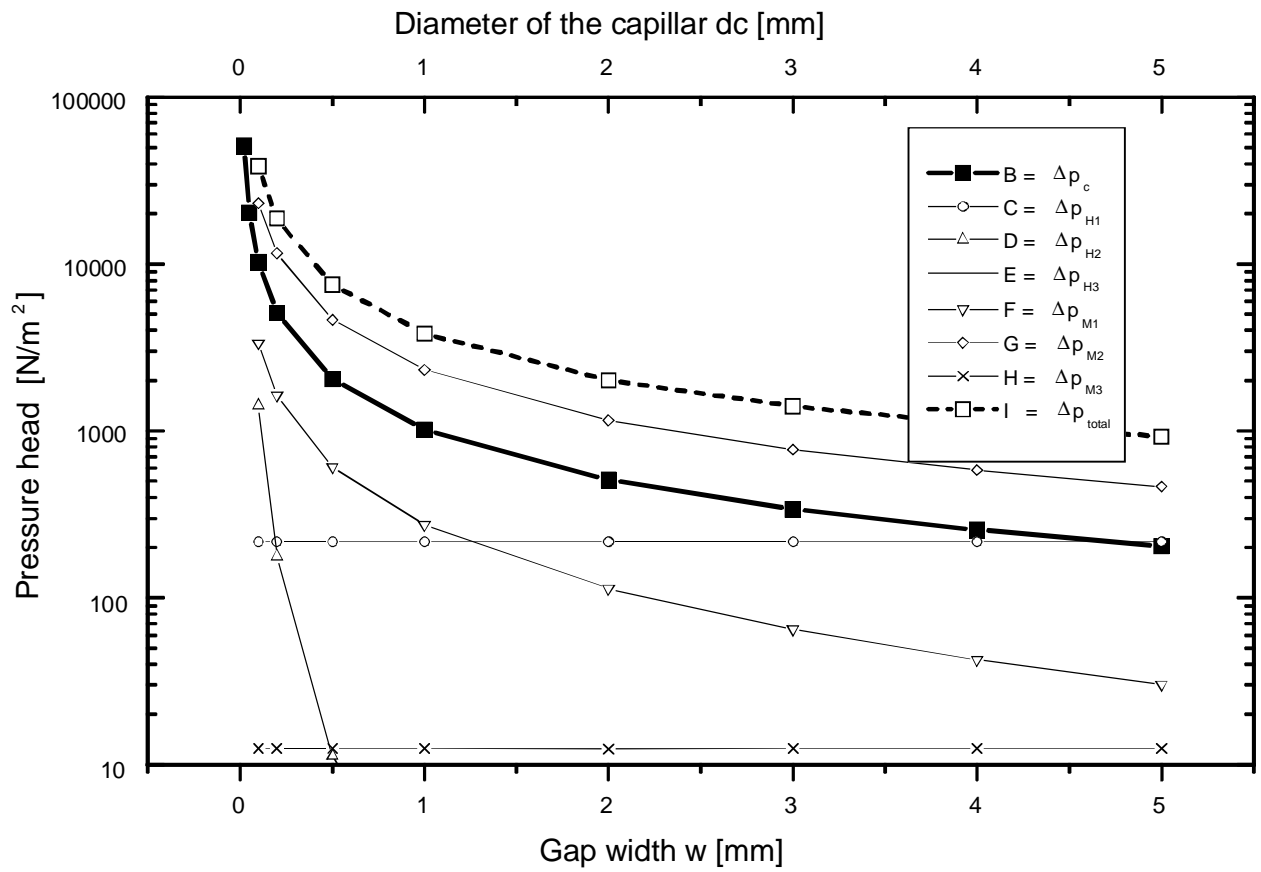


Fig. 2 Capillary pressure head, different pressure losses and the sum of the pressure losses in dependance of the capillary diameter d_c and of the gap width w respectively.

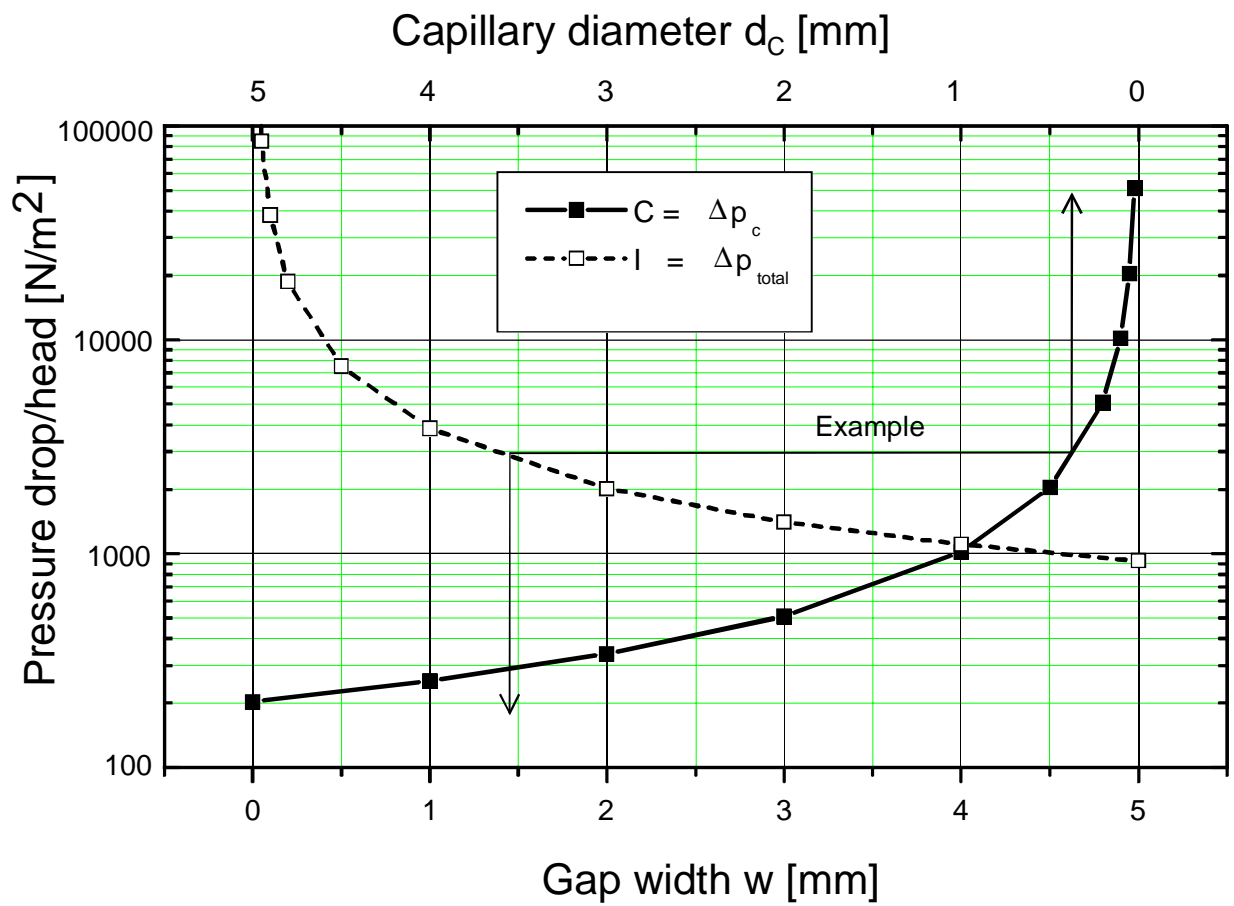


Fig. 3 Capillary pressure head and the total pressure drop in dependance of the capillar diameter d_C and of the gap width w respectively.