

# Processes Influencing PFAS Transport

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Managing Per- and Polyfluoroalkyl Substances (PFAS) at Your Site:  
Key Technical and Regulatory Issues

1:30-2:15 pm

Thursday, September 12, 2019

# Presentation Overview

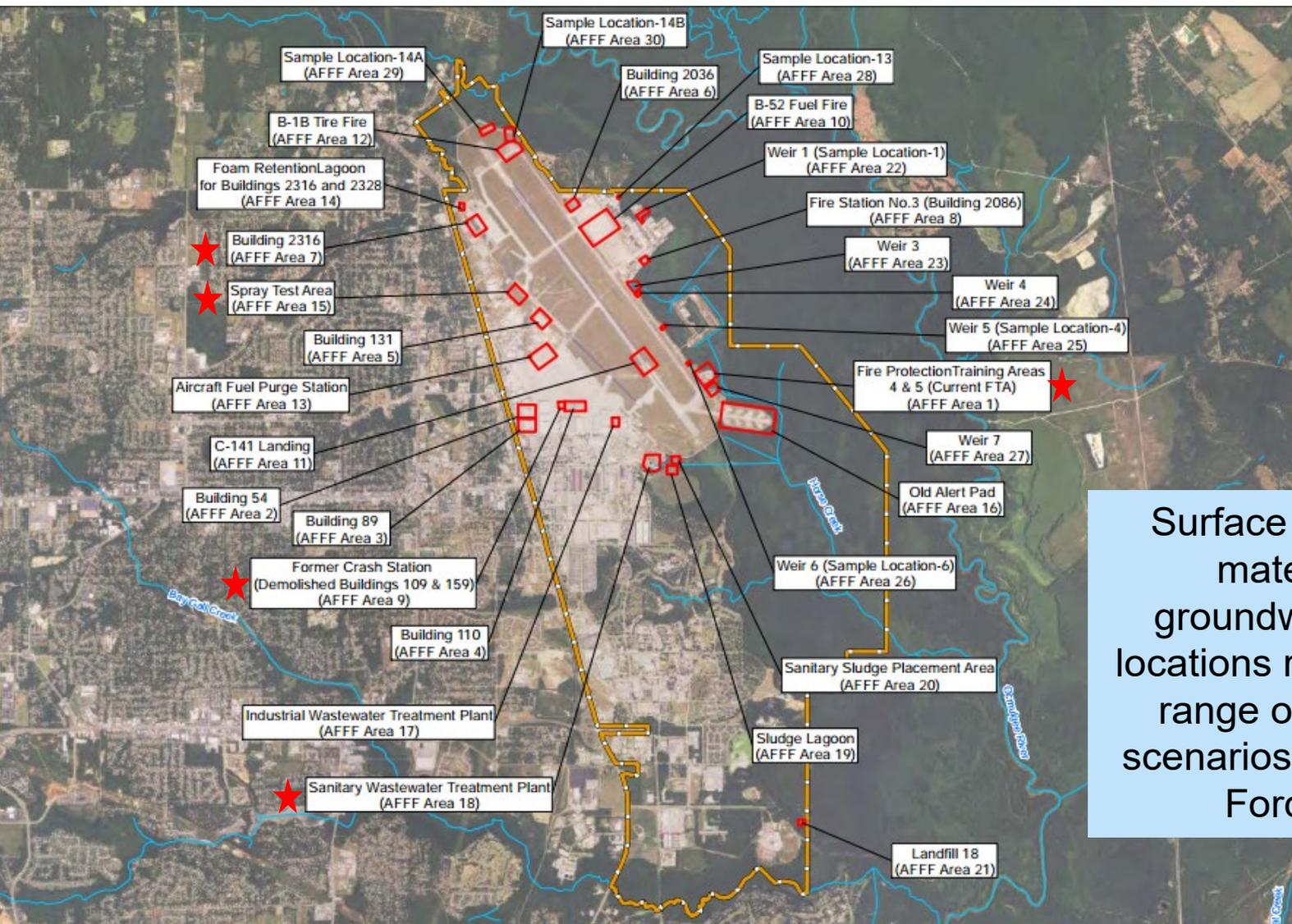
- AFFF Release Scenarios
- (Fluoro)Surfactant Properties and Behavior
- Interfacial Processes Impacting PFAS Transport
- In Situ PFAS Sequestration

# PFAS Release Scenario-AFFF Use and Training

Former Loring AFB, Limestone, ME

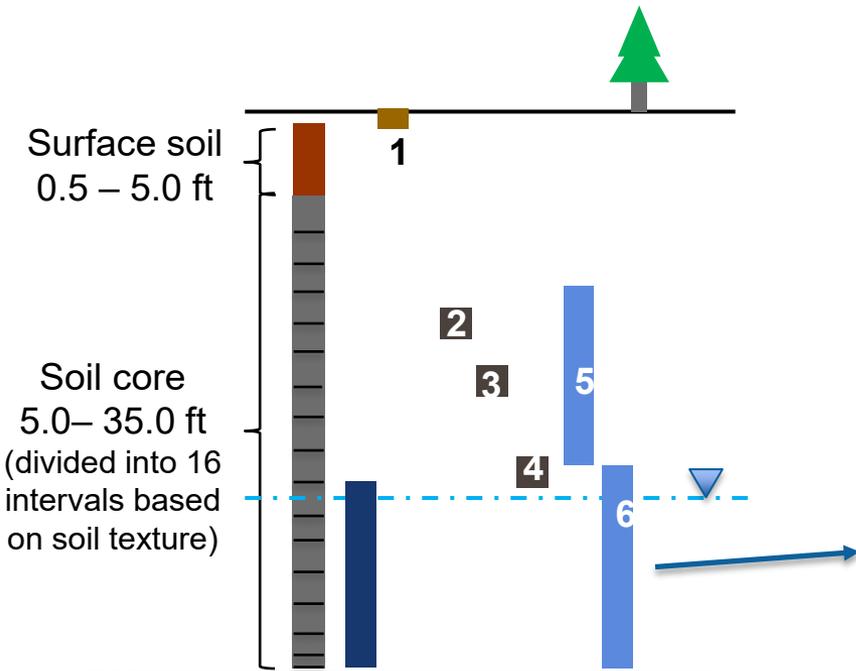


# AFFF-impacted Sites at Robins AFB (Georgia)



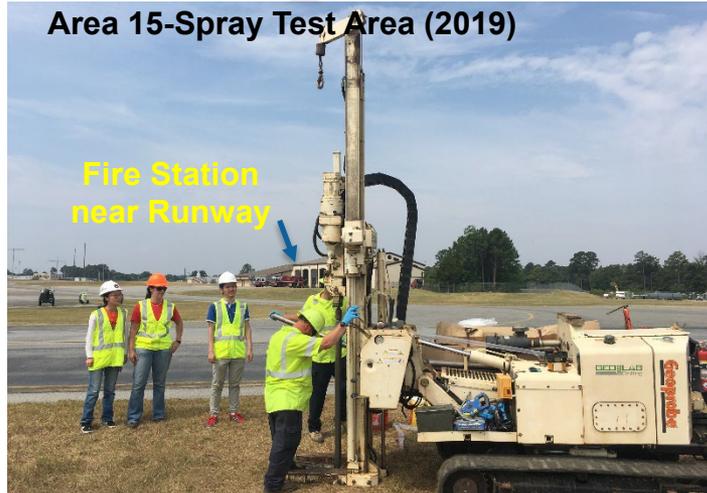
Surface soil, aquifer material and groundwater from 5 locations representing a range of AFFF spill scenarios at Robins Air Force Base

# Assess PFAS Concentration and Microbial Community Profiles



	Depth (ft)	PFBS	PFOA	PFOS
1	0 - 0.5	265.8 ± 490.2	34.5 ± 39.7	2705 ± 2149
2	17 - 18	5.2	0.66	4.4
3	19 - 20	0.66	0.66	2.4
4	26 - 27	37	17	44
5	15 - 25	3.4 ± 1.4	1.6 ± 0.2	22.7 ± 5.5
6	25 - 35	2.4	1.8	8.6

2017 samples (µg/kg for soil, µg/L for water)

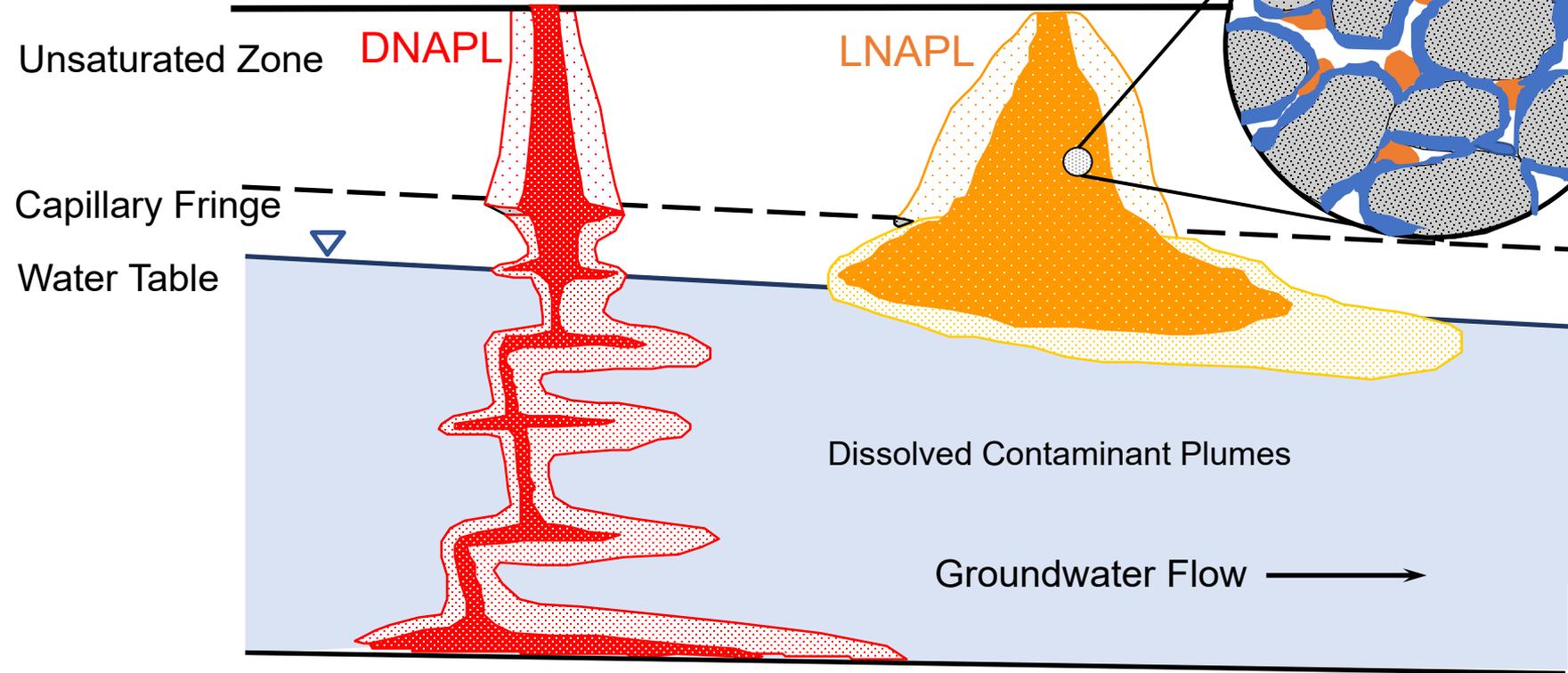
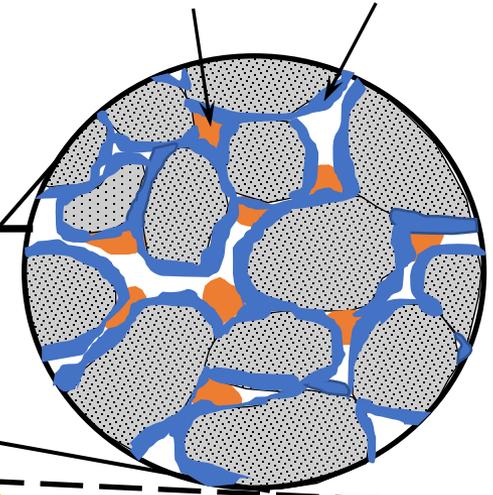


- Evaluate PFAS concentration and microbial communities as a function of soil properties
- Prepare microcosms to investigate precursor transformation rates and byproduct formation

# PFAS Release Scenario-Mixed Contaminants



Residual  
LNAPL      Water



Lower Confining Layer

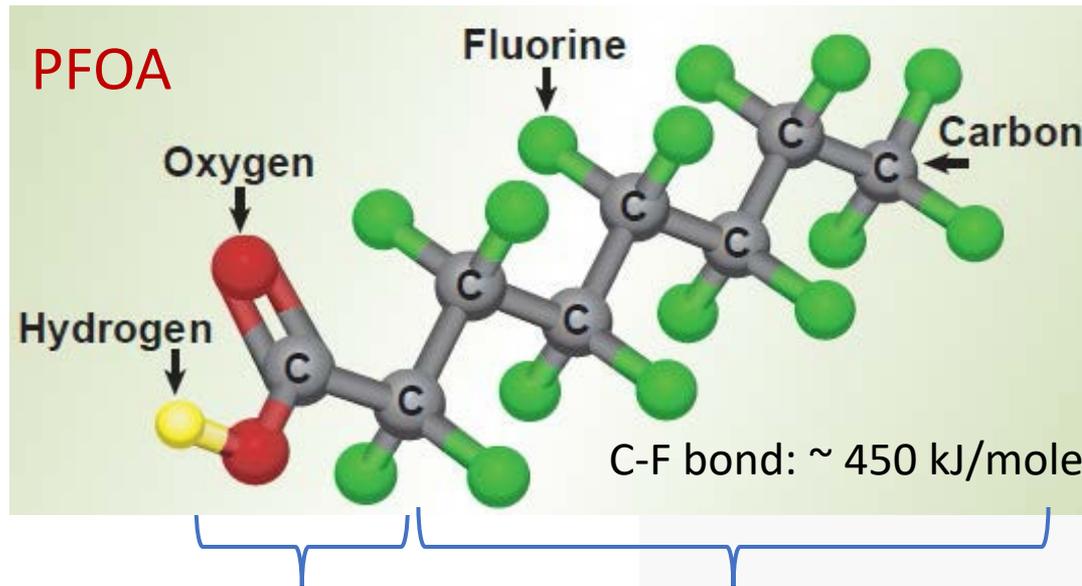
# (Fluoro)Surfactant Properties and Behavior

# Surface Active Agents (Surfactants)

## General Properties and Nomenclature:

- Amphiphilic (polar and nonpolar moieties): Hydrophilic “head” group + Hydrophobic “tail” group
- Strong tendency to accumulate at interfaces (air-water, NAPL-water)
- Individual molecules (monomers) self assemble to form micelles as the aqueous phase concentration is increased
- Classification is based on the polar head group:  
Anionic, Cationic, Nonionic, Amphoteric, Zwitterionic

# PFAS Classified as “Fluorosurfactants”



Hydrophilic “head” group

Hydrophobic/lipophilic “tail”

- Low Volatility
- Recalcitrant
- Foam/Emulsion Formation



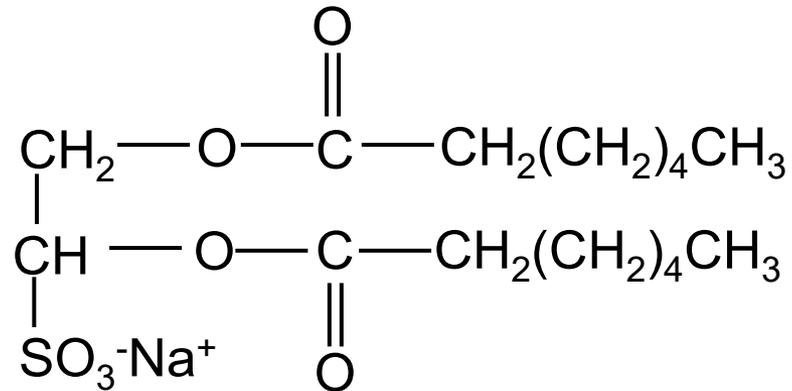
# Examples of Anionic Surfactants

Sodium dodecyl sulfate (SDS):



MW = 288 g/mole  
CMC = 2,100 mg/L

Sodium dihexylsulfosuccinate (SDHSS, Aersol MA-100):



MW = 388 g/mole  
CMC = 5,360 mg/L

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Perfluorooctanesulfonic acid (PFOS)



MW = 500 g/mole

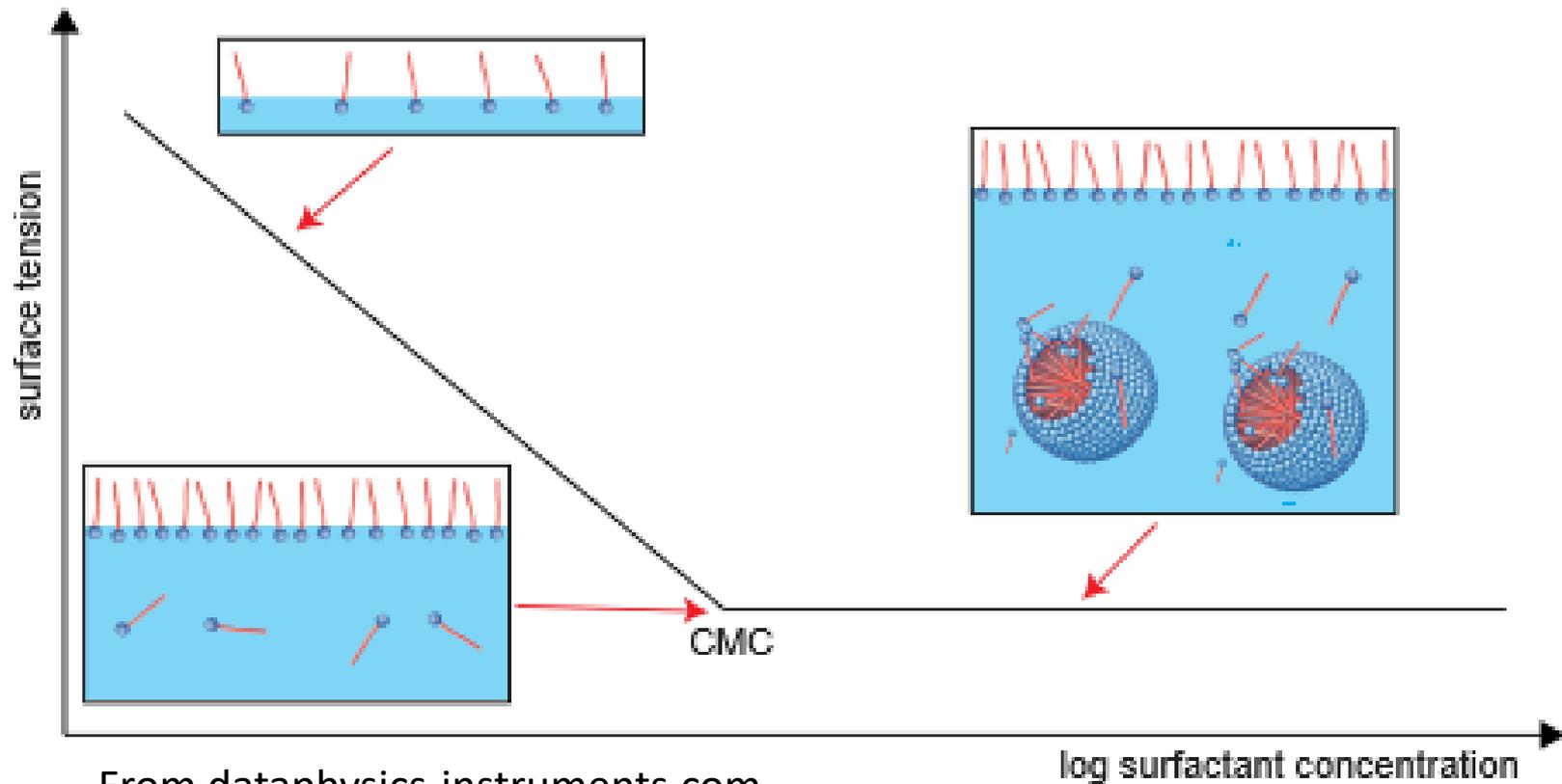


MW = 538 g/mole

CMC = 4,000-5,000 mg/L

...but the solubility is  
< 1000 mg/L???

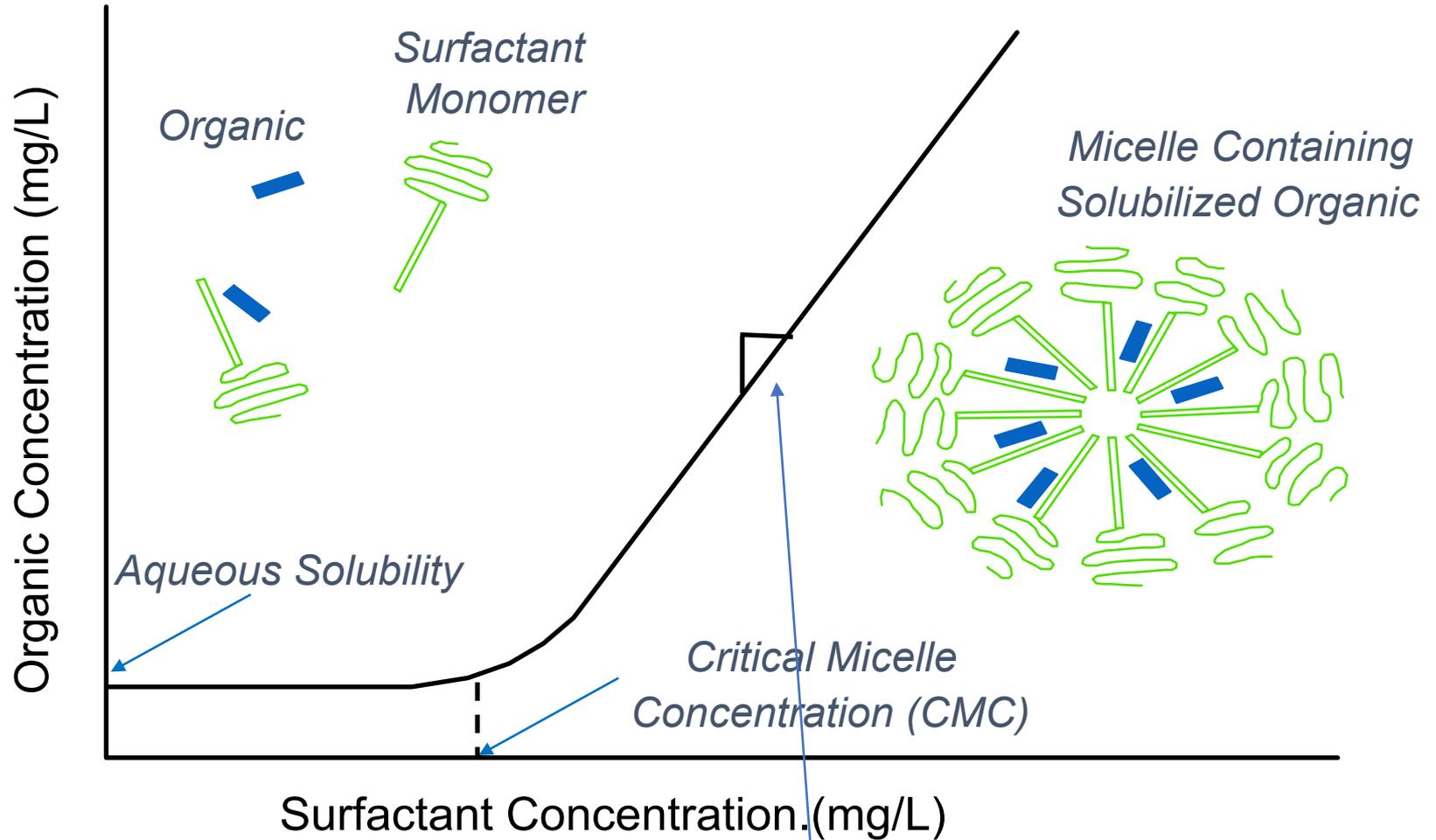
# Critical Micelle Concentration (CMC)



From [dataphysics-instruments.com](http://dataphysics-instruments.com)

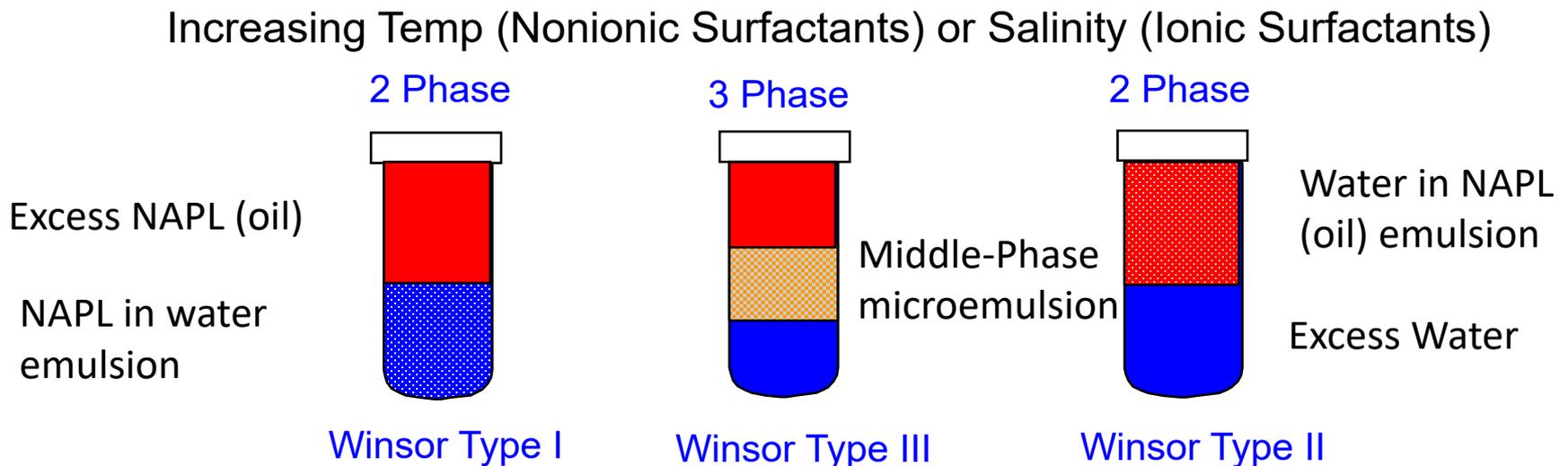
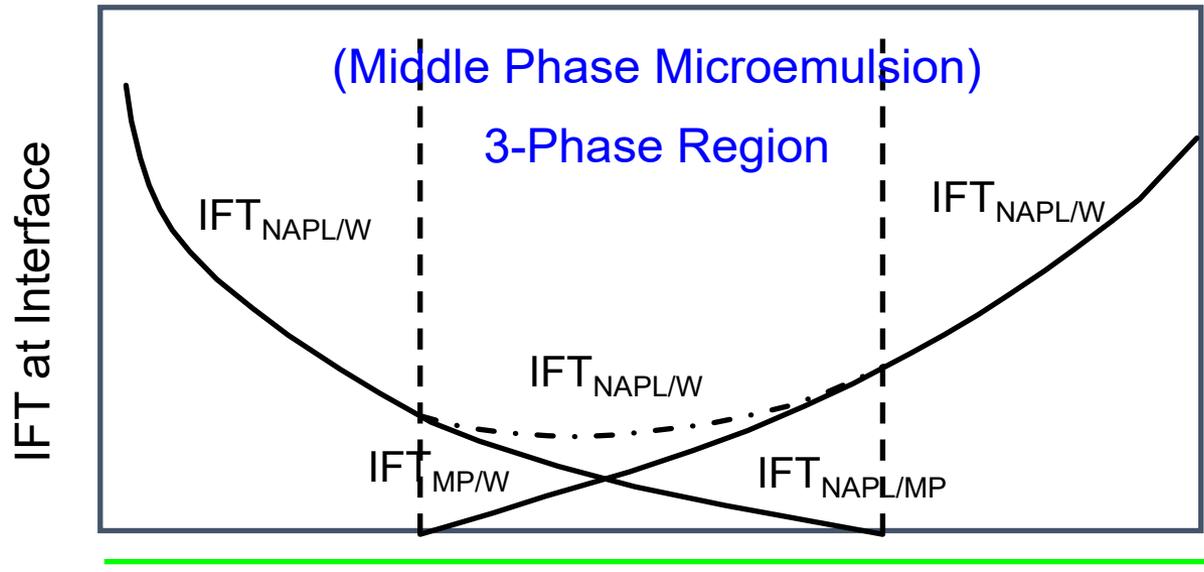
- At concentrations above the CMC, the number of monomers remains constant, while the number of micelles continues to increase
- The surface tension remains constant above CMC because the air-water interface is saturated

# Micellar Solubilization of Organic Compounds



Weight Solubilization Ratio (WSR)  $WSR = \frac{C_o - C_{o,cmc}}{C_{surf} - C_{surf,cmc}}$

# Surfactant Phase Behavior: NAPL-Water Interfacial Tension (IFT) and Emulsions



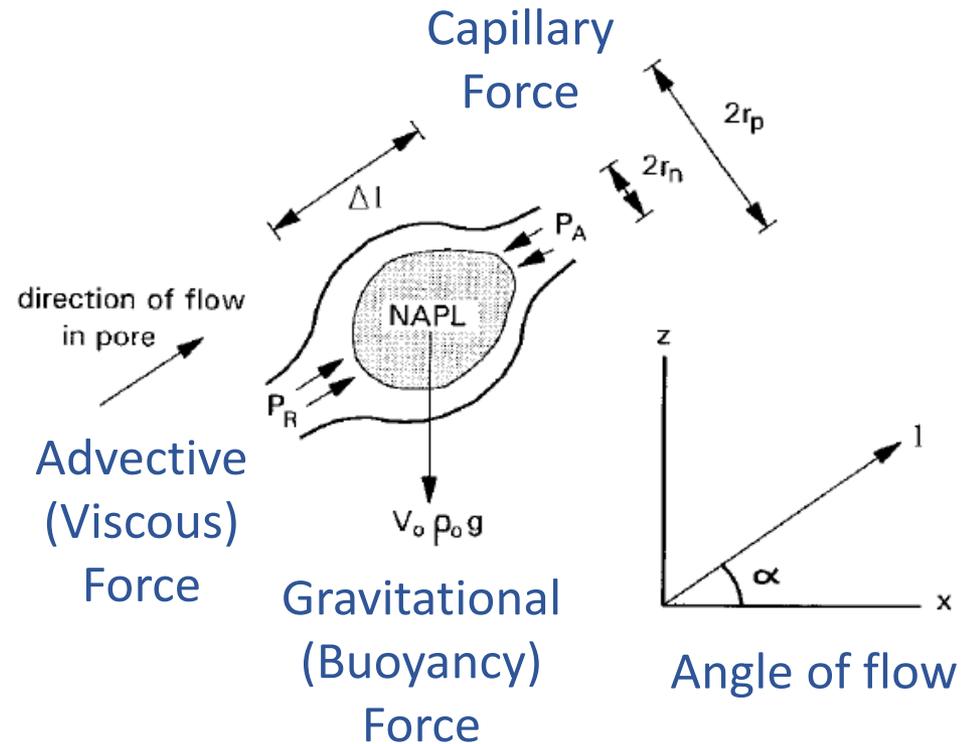
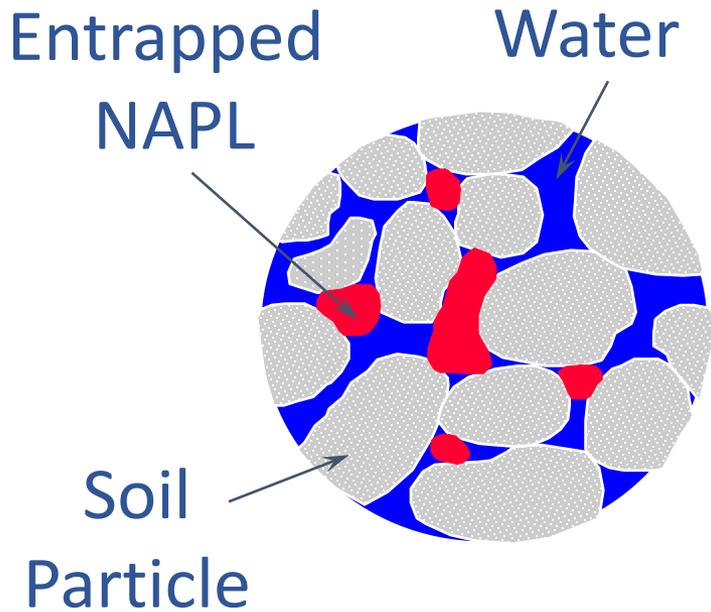
# Vertical Displacement (Mobilization) of PCE

Flushed with 4% Aerosol AY/OT (IFT = 0.09 dyne/cm)



# Determining Risk of NAPL Mobilization

## Total Trapping Number ( $N_T$ )



# Total Trapping Number ( $N_T$ )

*Capillary Number:*

(viscous forces)

$$N_{Ca} = \frac{q\mu}{\sigma_{ow} \cos \theta}$$

*Bond Number:*

(gravity forces)

$$N_B = \frac{\Delta\rho g k k_{rw}}{\sigma_{ow} \cos \theta}$$

$$N_T = \sqrt{N_{Ca}^2 + 2N_{Ca}N_B \sin \alpha + N_B^2}$$

*Vertical:*  $N_T = |N_{Ca} + N_B|$       *Horizontal:*  $N_T = \sqrt{N_{Ca} + N_B}$

$\mu$  = dynamic viscosity

$\Theta$  = contact angle

$k$  = intrinsic permeability

$k_{rw}$  = relative permeability to water

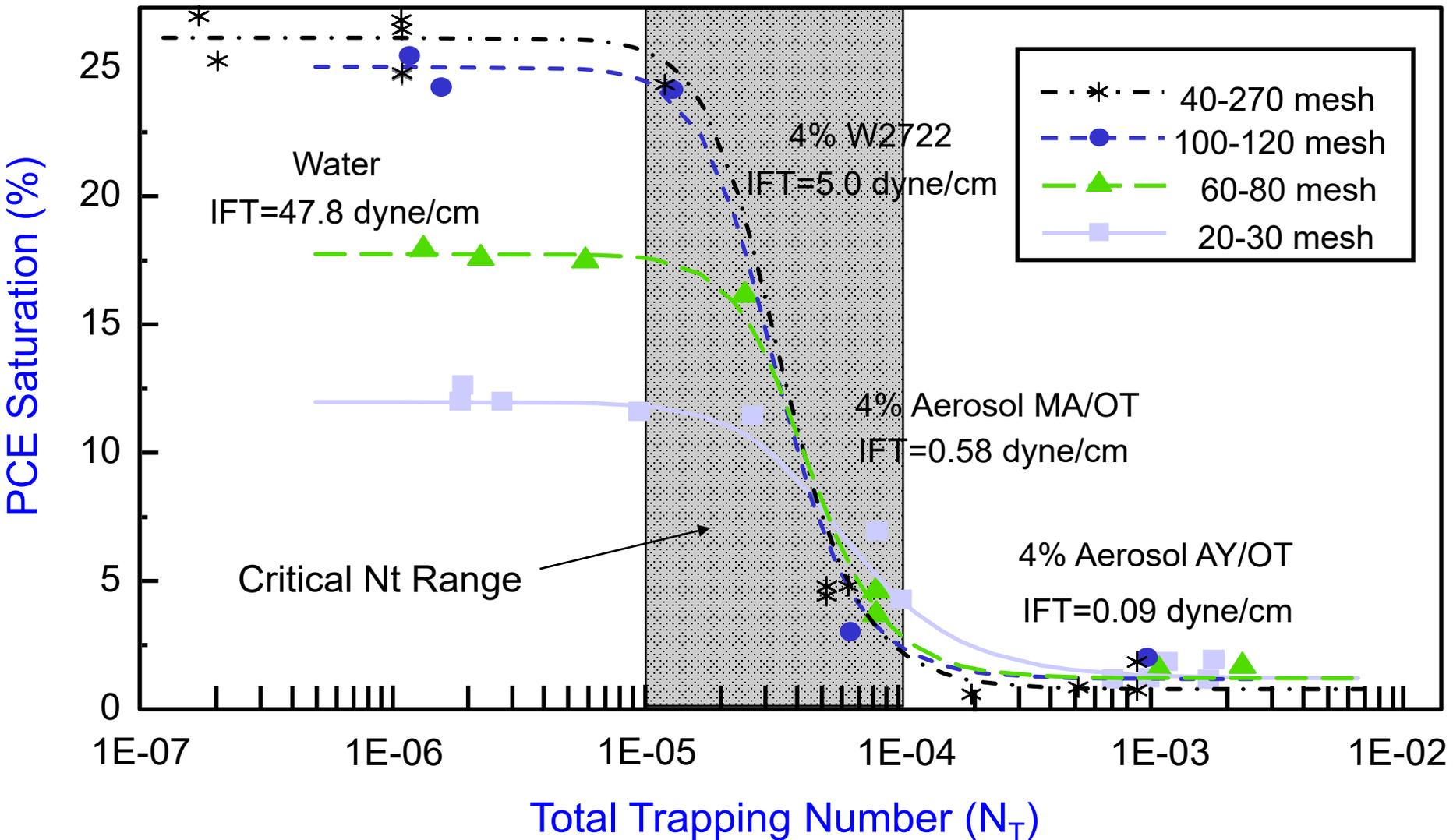
$\rho$  = density of fluid

$g$  = gravity constant

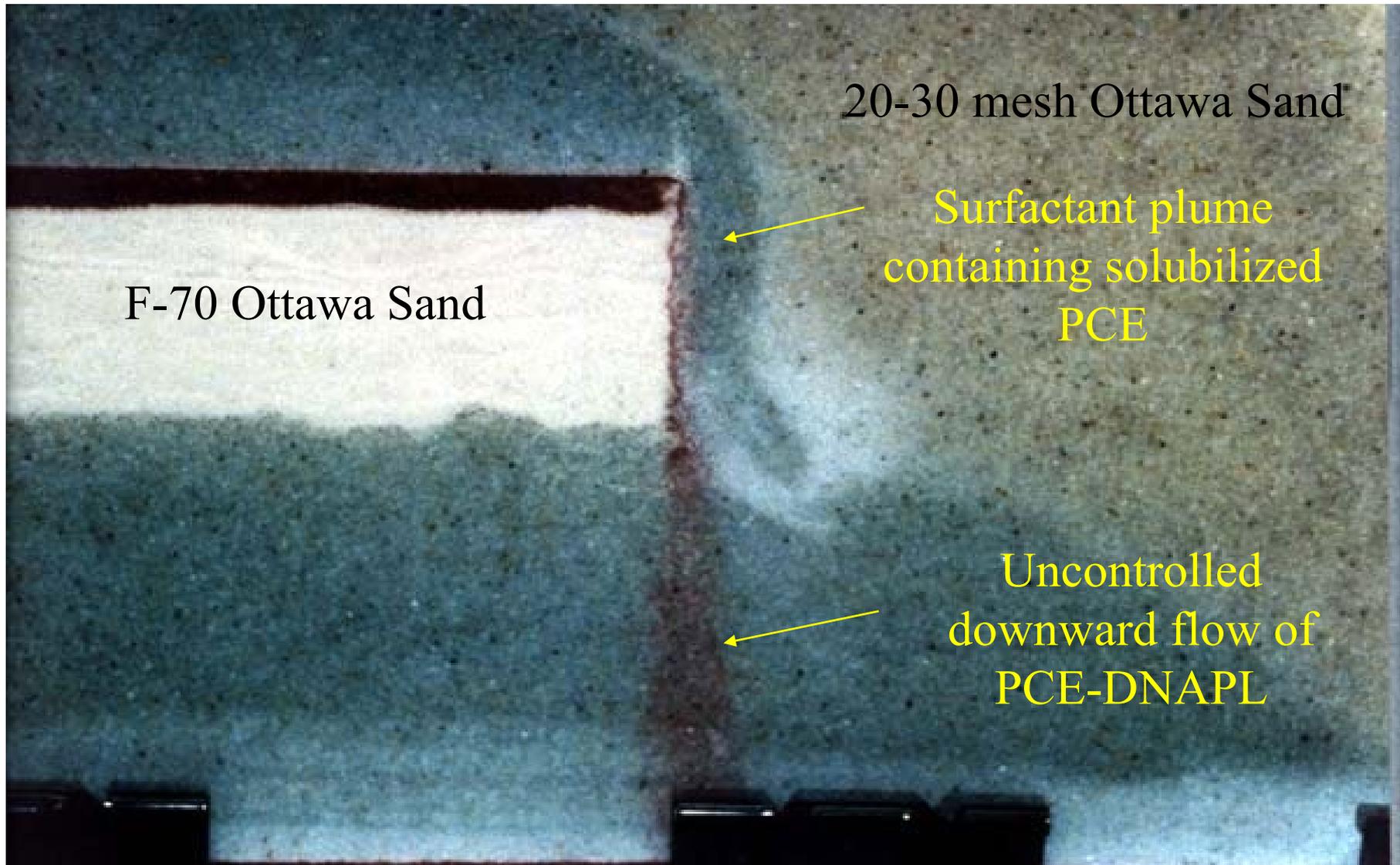
$q$  = Darcy velocity

$\sigma_{ow}$  = interfacial tension (oil-water)

# PCE Desaturation Curves for Ottawa Sands



# Risk of Uncontrolled DNAPL Mobilization



# Questions related to PFAS Transport

- How much PFAS accumulates at the air-water interface in unsaturated soils?
- How does PFAS impact soil water retention characteristics and water drainage during infiltration events?
- How does PFAS interact with NAPLs, and do these interactions result in enhanced NAPL solubility or mobilization?
- Can we modify existing mathematical models to describe PFAS fate and transport in complex systems?
- How do we account for mixtures of many surfactants, including PFAS?

# Interfacial Processes Impacting PFAS Transport

# Interfacial Tension Measurements

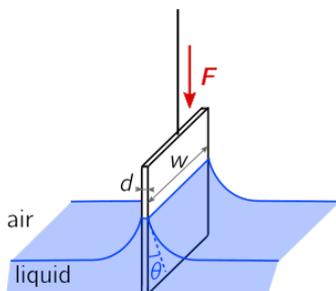
 **SERDP** Projects ER18-1149 and ER-2714  
DOD • EPA • DOE

## Sigma T700 Tensiometer

Resolution of  
0.01 mN/m

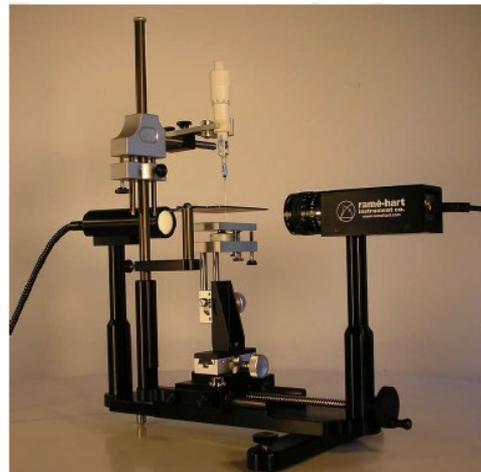


Note:  $\text{mN/m} = \text{dyne/cm} = \text{g/s}^2$

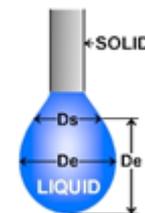


Surface Tension by  
Wilhelmy Plate

## Ramé-Hart Goniometer



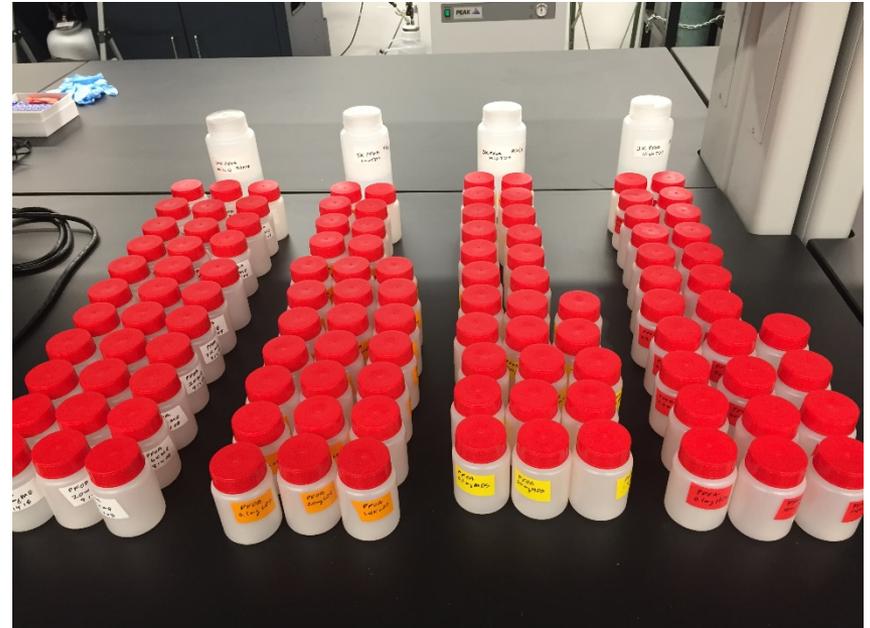
### Pendant Drop



Interfacial Tension by  
Pendant Drop

# Preparation of Solutions for IFT Measurements

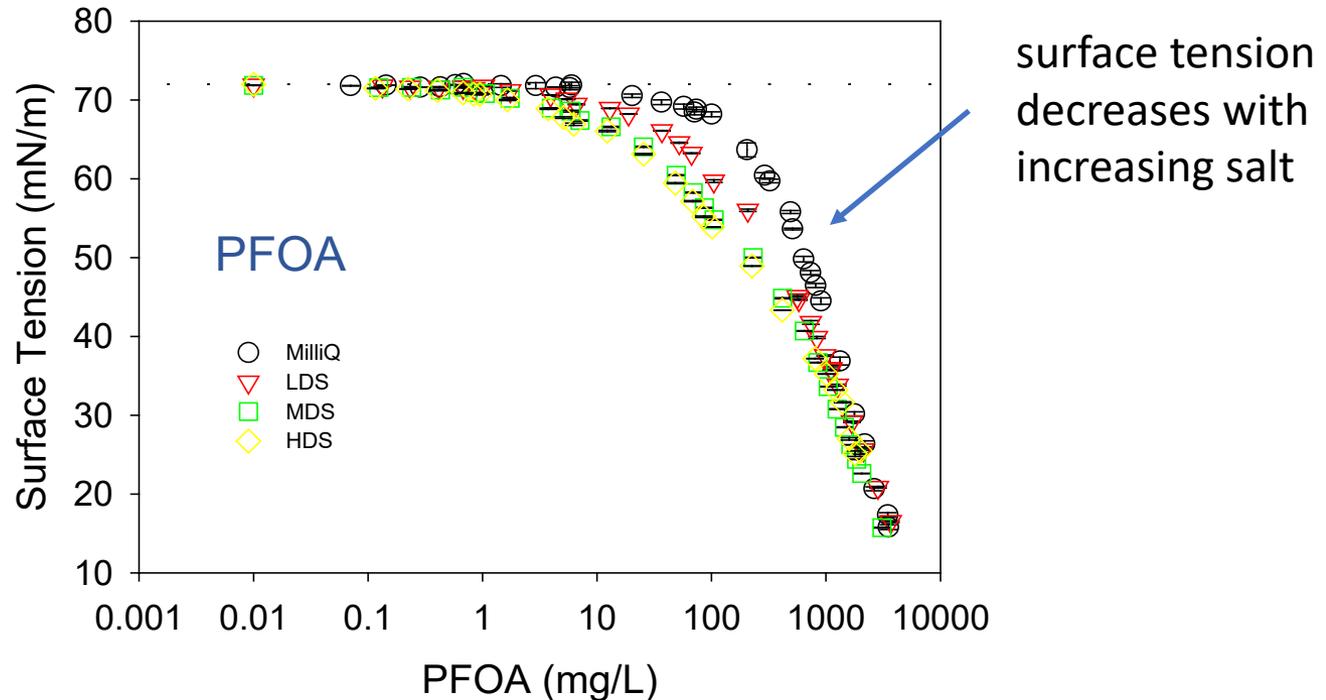
- Stock solutions ranged from 50 to 10,000 mg/L
  - PFOA or KPFOS solids using analytical balance
  - Sonicating for 30 min and heating overnight at 40 °C
- Concentrations from 0.1 to 50 mg/L prepared by serial dilution
- Concentrations verified by LC-MS/MS
- To simulate principal aquifers in US, aqueous solutions contained  $\text{MgSO}_4$ ,  $\text{NaHCO}_3$ ,  $\text{KCl}$ , and  $\text{CaCl}_2$ 
  - **Low Dissolved Solids (LDS)** ~40 mg/L (high purity drinking water) ~9 mM
  - **Mid Dissolved Solids (MDS)** ~400 mg/L (secondary drinking water standard) ~90 mM
  - **High Dissolved Solids (HDS)** ~1,700 mg/L (unpleasant drinking water) ~380 mM



PFOA and PFOS working solutions from 0.1 to 10,000 mg/L in 100-mL HDPE bottles

# Air-Water Interfacial Tension (Surface Tension)

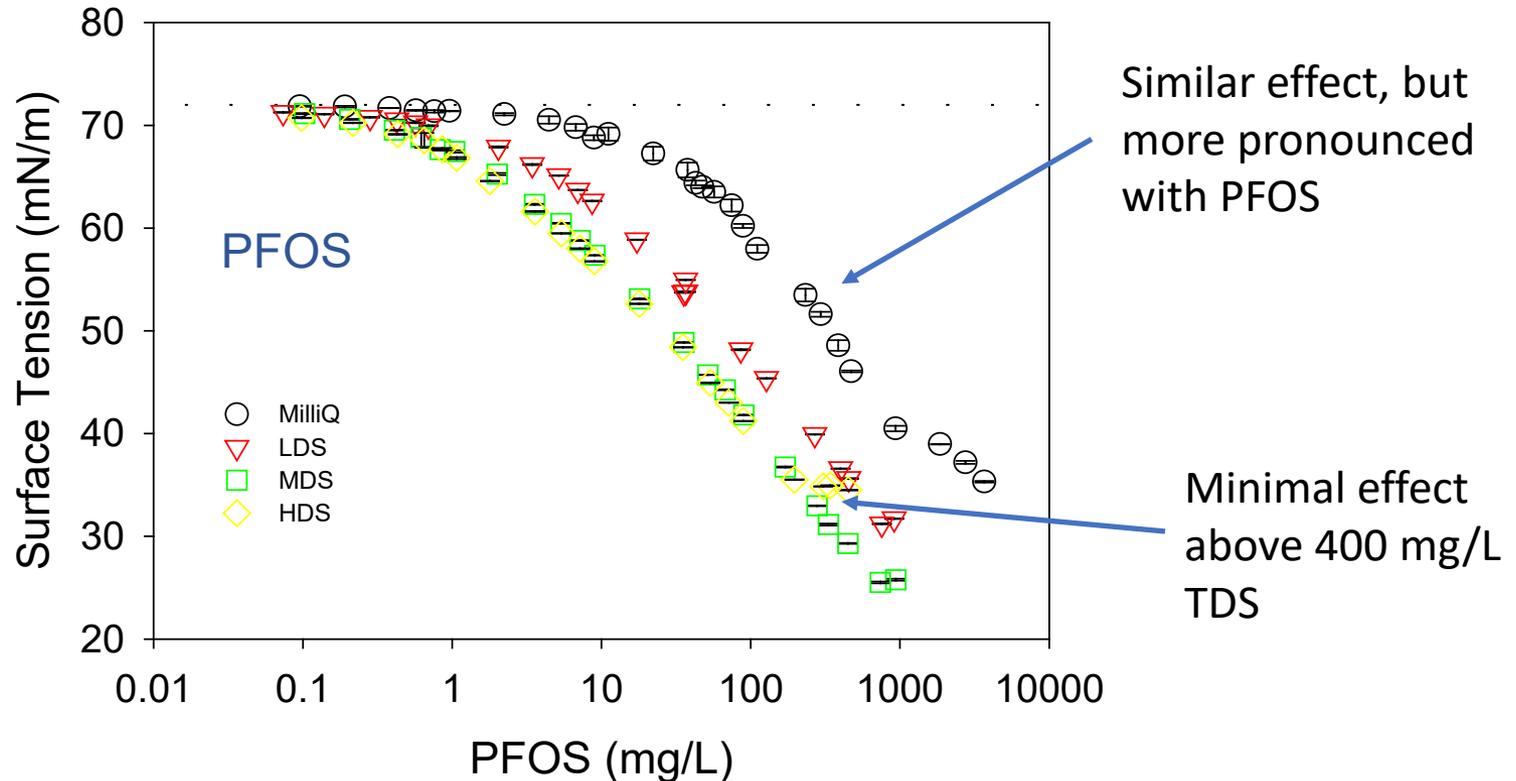
## PFOA (Effect of Salts)



- To simulate principal aquifers in US Background solution contains  $\text{MgSO}_4$ ,  $\text{NaHCO}_3$ ,  $\text{KCl}$ , and  $\text{CaCl}_2$
- Dissolved salts resulted in lower surface tension for PFOA
  - **Low Dissolved Solids (LDS)** ca. 40 mg/L (high purity drinking water)
  - **Mid Dissolved Solids (MDS)** ca. 400 mg/L (secondary drinking water standard)
  - **High Dissolved Solids (HDS)** ca. 1,700 mg/L (unpleasant drinking water)

# Air-Water Interfacial Tension (Surface Tension)

## PFOS (Effect of Salts)



- **Low Dissolved Solids (LDS)** ca. 40 mg/L (high purity drinking water)
- **Mid Dissolved Solids (MDS)** ca. 400 mg/L (secondary drinking water standard)
- **High Dissolved Solids (HDS)** ca. 1,700 mg/L (unpleasant drinking water)

# Gibb's Equation → Surface Excess

Interfacial tension is a measure of surface concentration or surface “excess” ( $\Gamma$ ) [Langmuir, 1917]

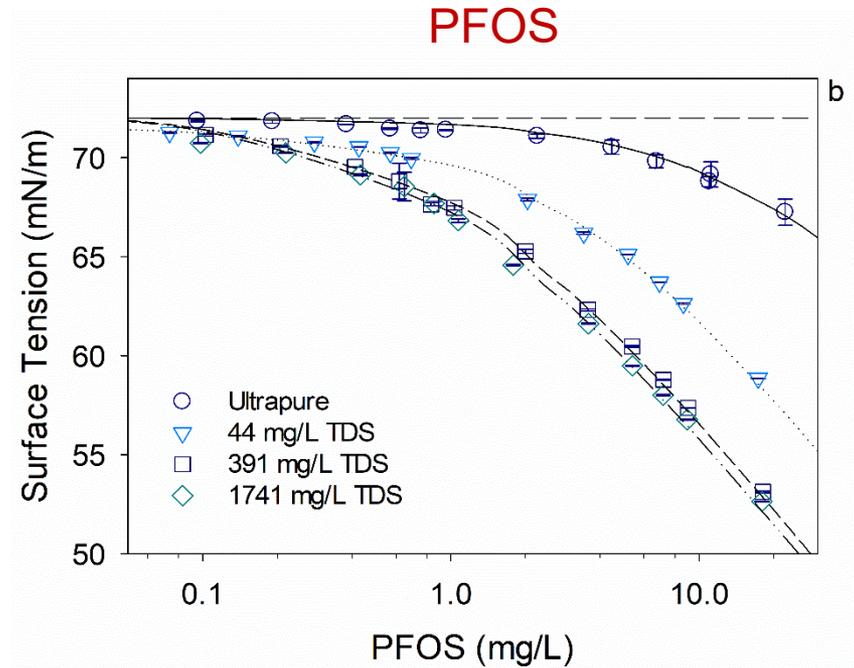
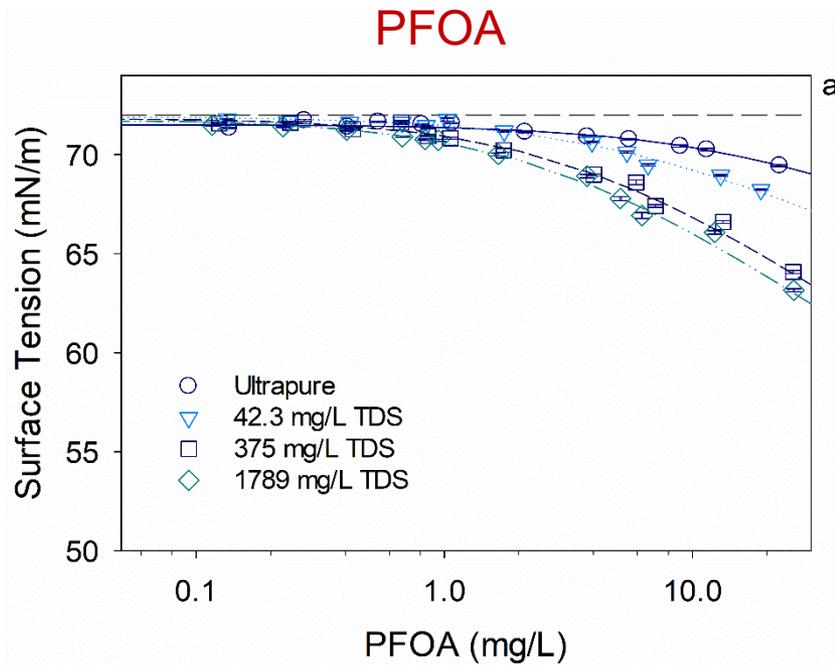
$$\Gamma = -\frac{C}{RT} \left( \frac{\partial \gamma}{\partial C} \right)_T \longrightarrow \gamma = \gamma_0 \left[ 1 - a * \ln \left( \frac{C}{b} + 1 \right) \right] \longrightarrow \Gamma = \frac{a\gamma_0}{RT} \frac{C}{C + b}$$

Gibb's Equation                      Szyszkowski Equation                      Langmuir/Szyszkowski Eq.

$\Gamma$  = surface excess  
 $\gamma$  = surface tension  
 $C$  = aqueous conc.  
 $R$  = gas constant  
 $T$  = temperature (°K)

- “a” and “b” are nonlinear fitting parameters
- This equation allows you to fit the entire surface tension vs. PFAS concentration curve

# Langmuir/Szyszkowski Equation



$$\Gamma = -\frac{C}{RT} \left( \frac{\partial \gamma}{\partial C} \right)_T$$

Gibb's Eq.



$$\gamma = \gamma_0 \left[ 1 - a \ln \left( \frac{C}{b} + 1 \right) \right]$$

Szyszkowski Eq. Fit



$$\Gamma = \frac{a\gamma_0}{RT} \frac{C}{C + b}$$

Langmuir/Szyszkowski Eq.

# Surface Excess Calculations

## Equation Development

$K_i$  = Linear Partition Coefficient  
(L/m<sup>2</sup>)

$$\Gamma = -\frac{C}{RT} \left( \frac{\partial \gamma}{\partial C} \right)_T \longrightarrow K_i = \frac{1}{RT} \frac{\partial \gamma}{\partial C} \longrightarrow \Gamma = K_i C_w \quad \text{Linear}$$

$$\Gamma = -\frac{1}{RT} \left( \frac{\partial \gamma}{\partial \ln C} \right)_T \longrightarrow K_i = \frac{1}{RT} \frac{\partial \gamma}{\partial \ln C} \longrightarrow \Gamma = K_i \frac{C_w}{C_{ref}} \quad \text{Natural Log}$$

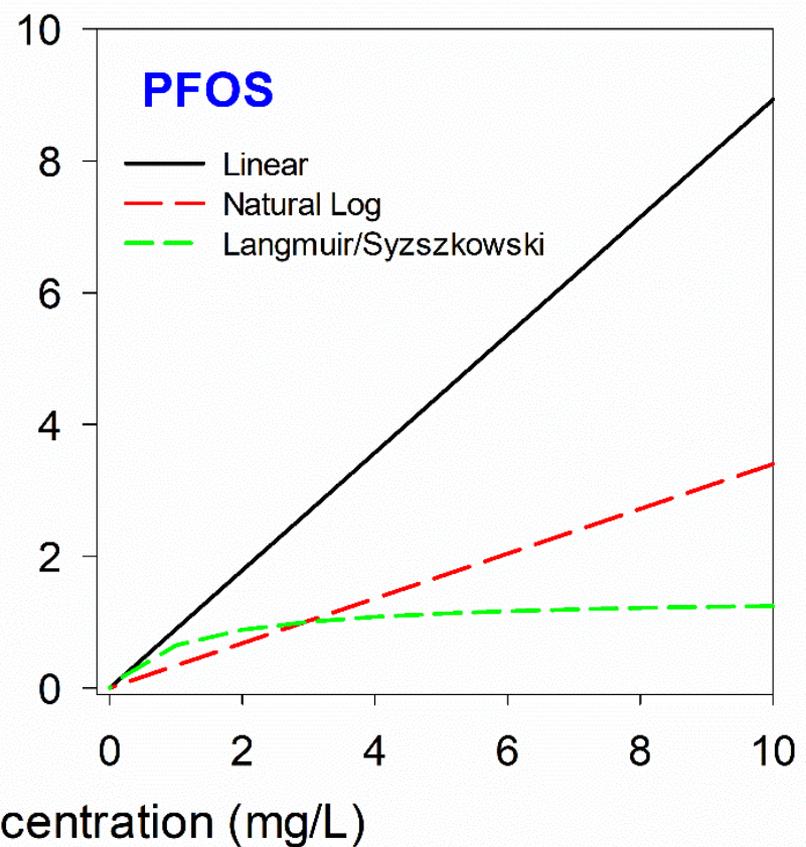
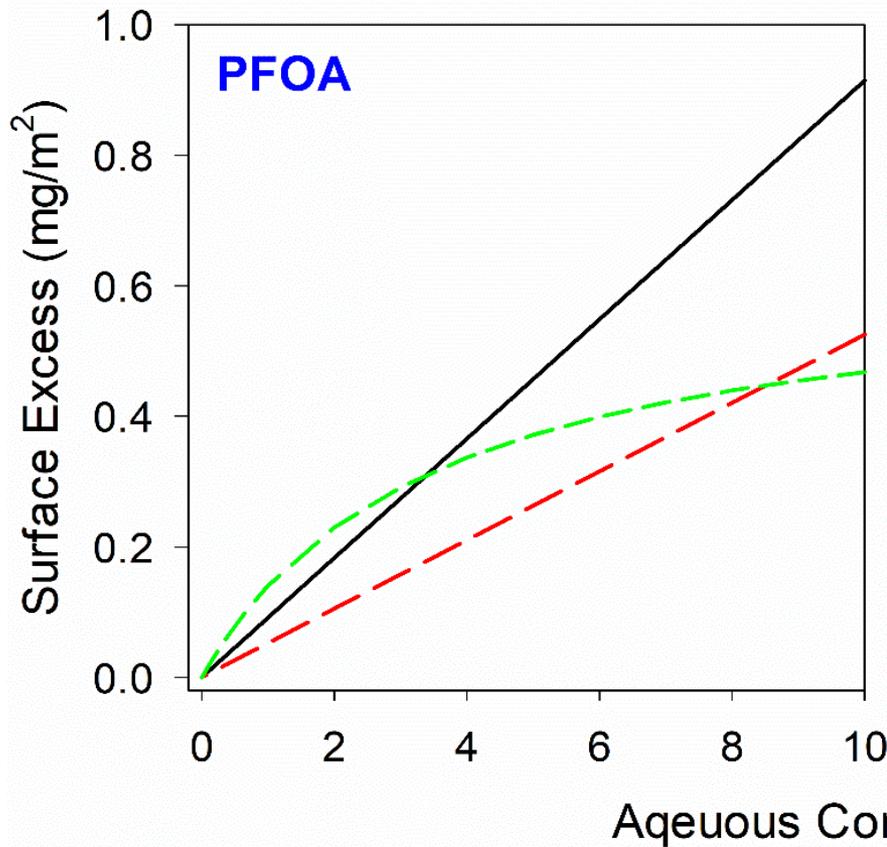
$K_i$  = Natural Log Partition Coefficient  
(mg/m<sup>2</sup>)

*requires an arbitrary reference conc.*  
(e.g., Lyu et al., 2018,  $C_{ref} = 1$  mg/L)

$$\Gamma = \frac{a\gamma_0}{RT} \frac{C}{C + b} \quad \text{Nonlinear} \\ \text{(Langmuir/Szyszkowski)}$$

# Surface Excess Calculations

## Comparison of Different Approaches



$$\Gamma = K_i C_w$$

Linear

$$\Gamma = K_i \frac{C_w}{C_{ref}}$$

Natural Log

$$\Gamma = \frac{a\gamma_0}{RT} \frac{C}{C + b}$$

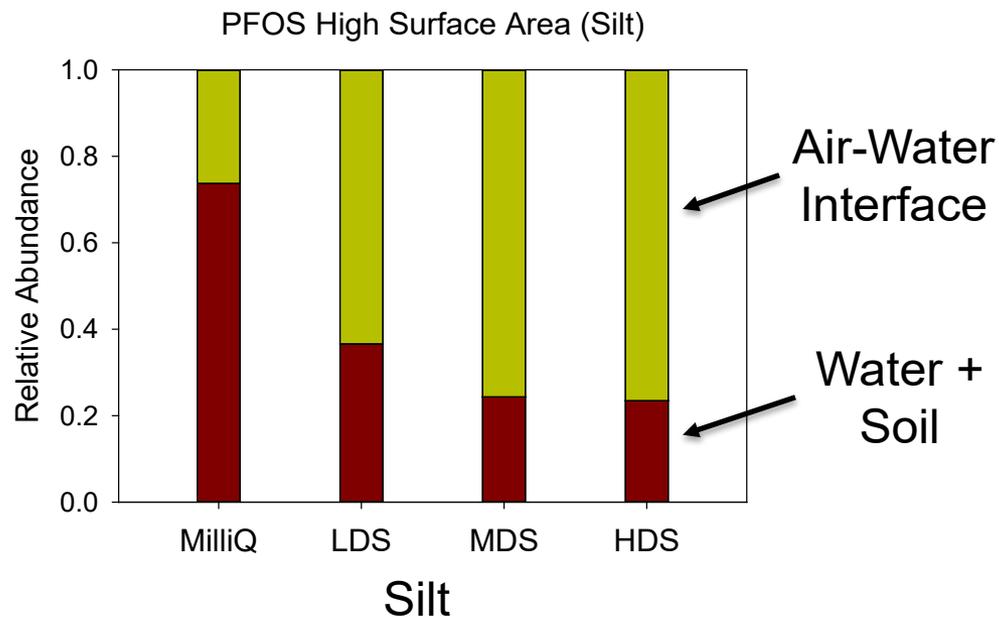
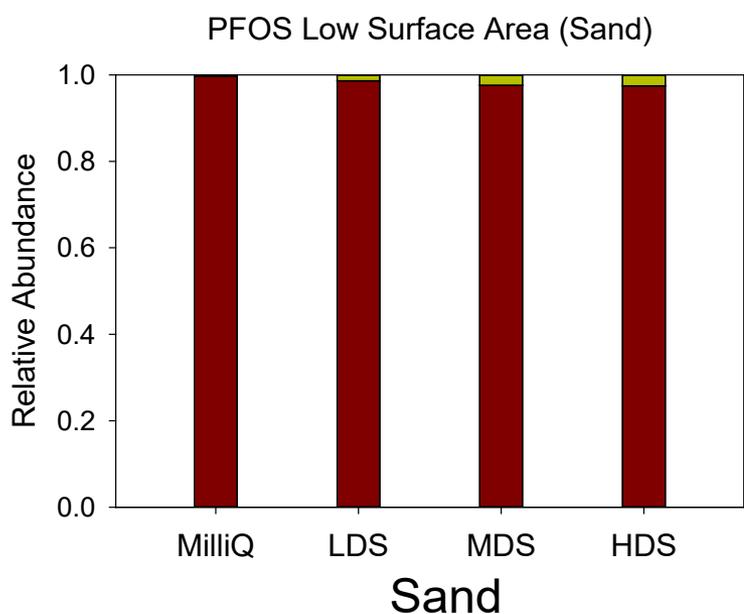
Langmuir/Szyszkowski

# PFOS Phase Distribution in Unsaturated Soils

Nonlinear: Langmuir/Szyszkowski Equation)

Total PFOS Mass = Mass in Water + Mass on Solids + Mass at Air-Water Interface

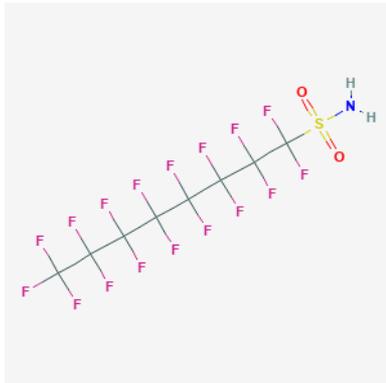
$$M_{\text{Total}} = V_T(C_w S_w + C_w K_D \rho_b + S_a \frac{a\gamma_0}{RT} \frac{C}{C+b})$$



- $C_w = 1$  mg/L,  $S_w = 0.26$ ,  $K_D = 1.14$  mg/kg,  $\rho_b = 1.5$  kg/L,  $S_a = 80$  cm<sup>-1</sup> sand,  $S_a = 1000$  cm<sup>-1</sup> silt (Brusseau, 2018)

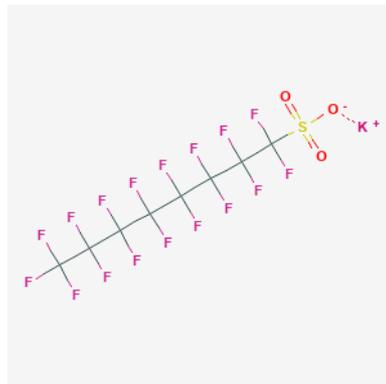
# Surface Tension of “PFOS” Mixture

Nonionic



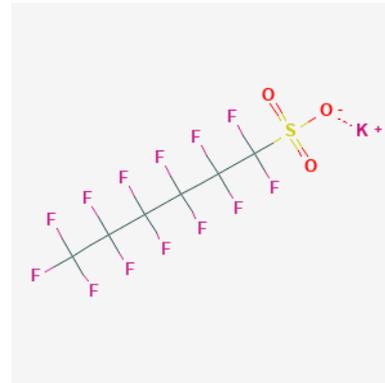
Perfluorooctane  
sulfonamide  
(FOSA)  
 $C_8F_{17}SO_2NH_2$

Ionic



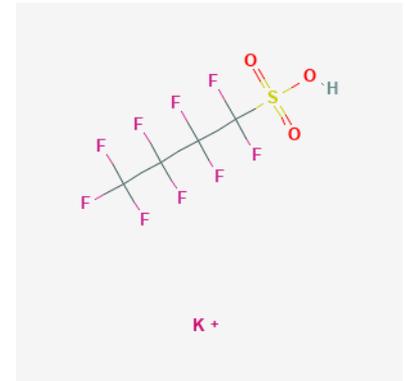
KPFOS  
 $C_8F_{17}SO_3K$

Ionic



KPFHxS  
 $C_6F_{13}SO_3K$

Ionic

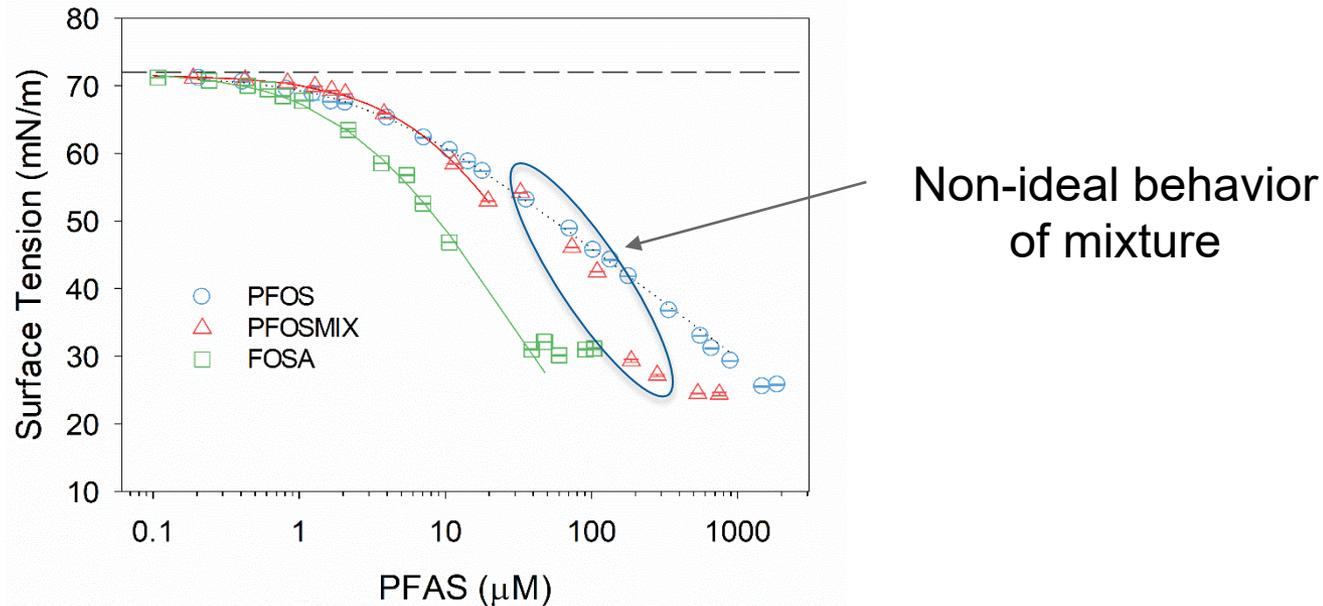


KPFBS  
 $C_4F_9SO_3K$

“PFOS mixture” consists of a sulfonamide and three sulfonates

- Prepared equimolar stock mixtures from solids with total concentrations of 100, 200, 400, and 600 mg/L
- Dilutions of stock mixtures in range from 0.1 to 80 mg/L
- Solutions in ultrapure water, and water with low, mid, and high dissolved solids

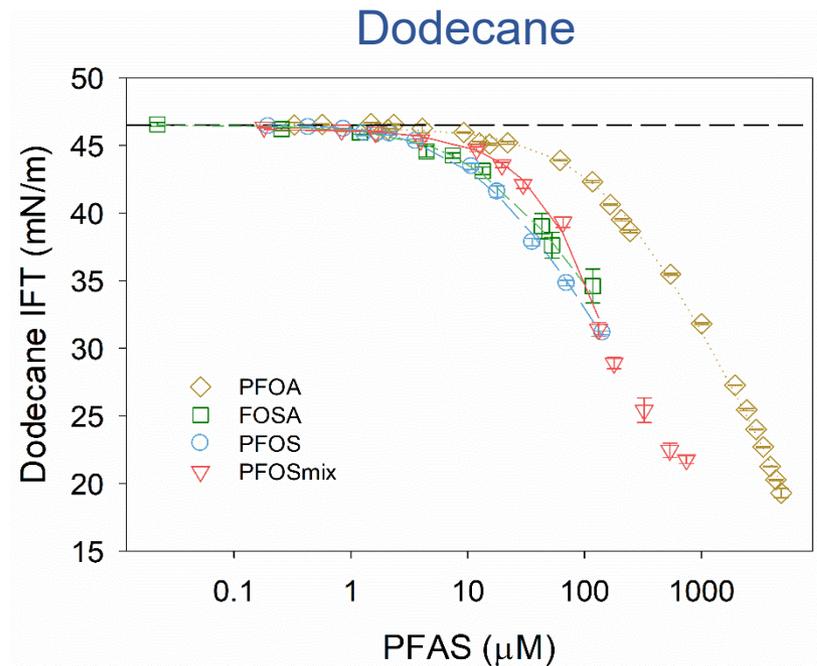
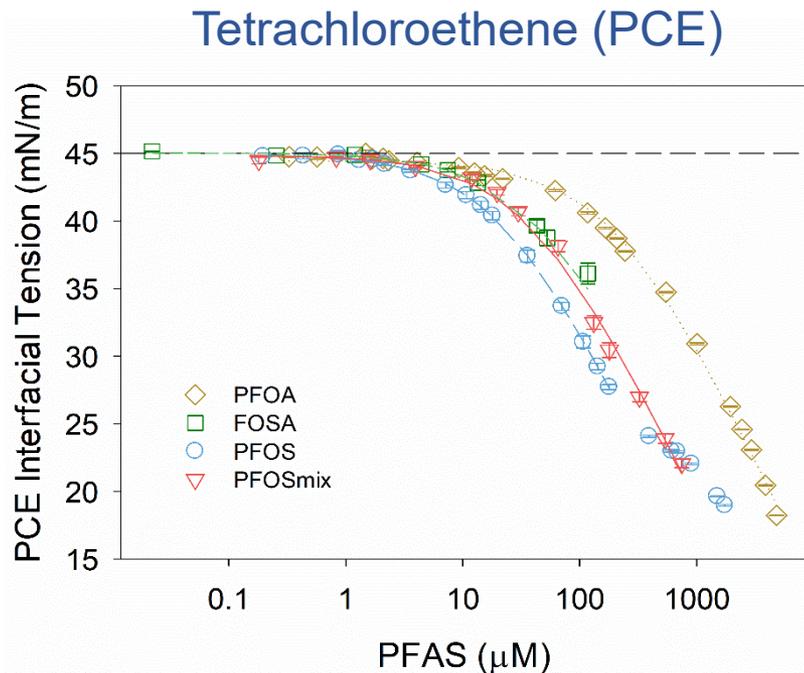
# Effect of PFAS Mixtures on Surface Tension Measurements



“PFOS mixture” contained a sulfonamide and three sulfonates in ca. 400 mg/L TDS

- PFBS, PFHxS, PFOS and FOSA (0.3:0.3:0.2:0.2 mole fractions)
- PFBS and PFHxS surface tension of 70 mN/m at 100 mg/L (not surface active)
- FOSA surface tension lowest at equivalent concentration
- PFOS mixture exhibited “ideal” surface tension behavior from 0.2 to 20 μmol/L, non-ideal at increasing concentrations

# NAPL-Water Interfacial Tension



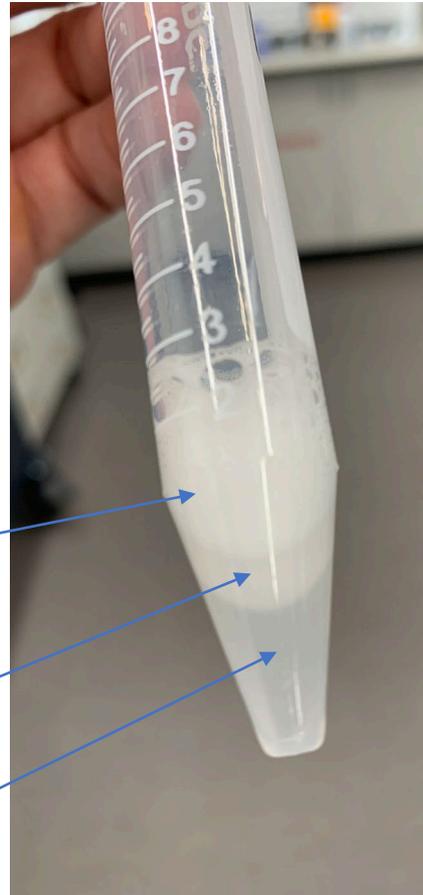
Drop of NAPL suspended in solutions containing PFAS with ca. 1700 mg/L TDS

Confirmed oleophobic nature of the perfluorocarbon chain (Moody and Field, 2000)

- Significant reduction in interfacial tension only observed for concentrated solutions (>100 mg/L)
- IFTs less than 5 mN/m (dyne/cm) typically needed for NAPL mobilization

# AFFF Phase Behavior

JP4 Jet Fuel



Foam

Macroemulsion

Aqueous Phase



4 mL : 4 mL

# AFFF Phase Behavior

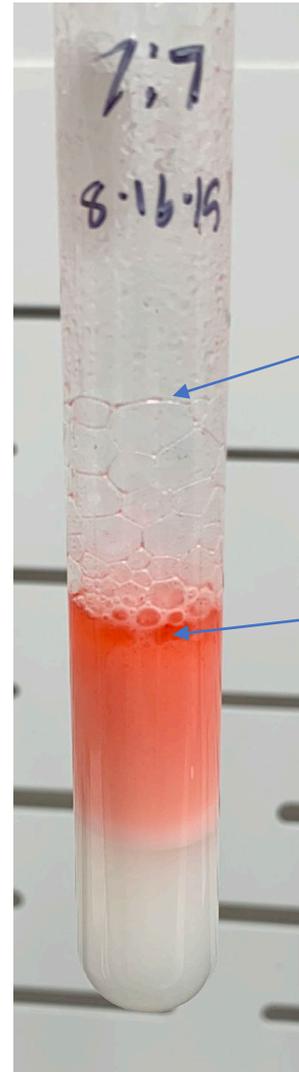
JP4 Jet Fuel (Oil Red O)



Foam

Macroemulsion

Aqueous Phase



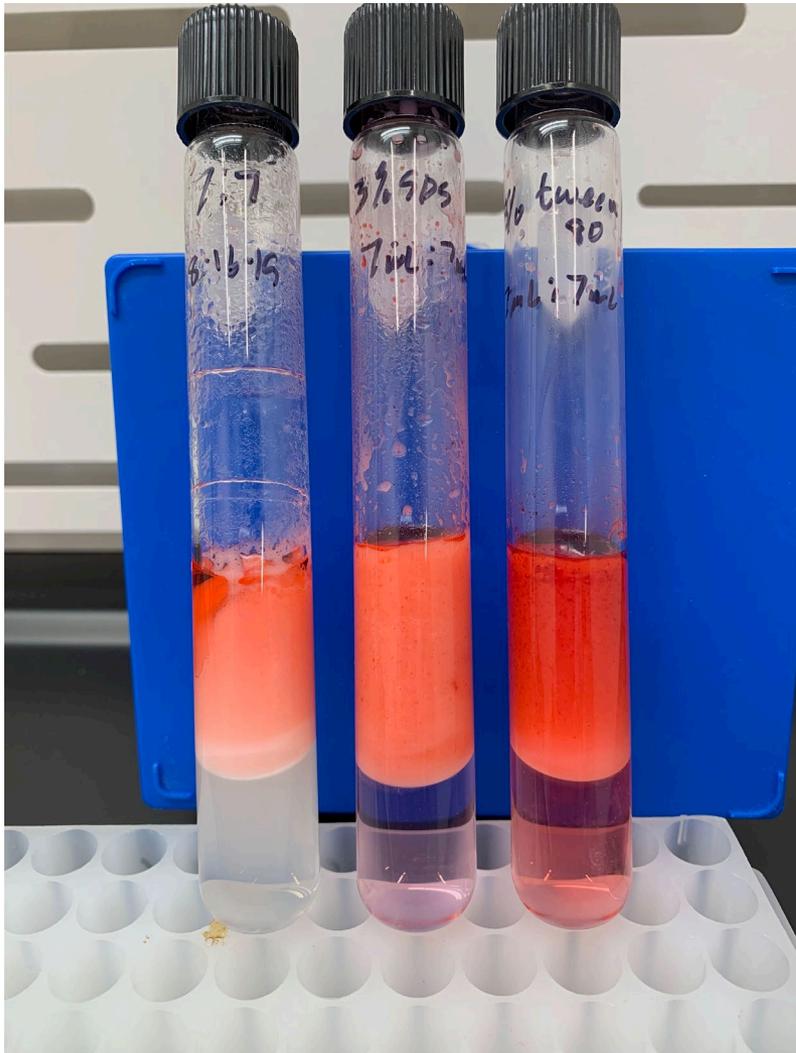
Collapsed Foam

JP4-NAPL

# Comparison AFFF Phase Behavior

## JP4 Jet Fuel

3M      SDS      Tween 80



- 3% active ingredient
- 7 mL JP-4 : 7 mL surfactant solution
- After 24 hr settling

# Mathematical Modeling of PFAS Transport in the Unsaturated Zone

# Modeling PFAS Adsorption at Air-Water Interface

**Objective:** Incorporate nonlinear PFAS adsorption at air-water interface using a modified version of Hydrus 1D

Richards Equation: 
$$\frac{\partial \theta}{\partial t} = \nabla \cdot (k \cdot \nabla h) + \frac{\partial k}{\partial z} + S$$

$$\frac{\partial}{\partial t} (\phi s_{\alpha} C_i^{\alpha}) + \nabla \cdot \phi s_{\alpha} (C_i^{\alpha} V^{\alpha} - D_i^{h^{\alpha}} \nabla C_i^{\alpha}) = \phi \sum_{\beta} E_{\alpha\beta_i} + R_i^{\alpha}$$

$$E_{ai}^i = -A_{ai} \frac{\partial \Gamma^i}{\partial t}$$

Langmuir Isotherm: 
$$\Gamma^i = \frac{a \gamma_0 C^i}{RT C^i + b}$$

*a* and *b*: Szyszkowski eq. parameters fitted using batch experimental results

Linear Isotherm: 
$$\Gamma^i = K_i C^i$$

$K_i$ : linear partitioning coefficient

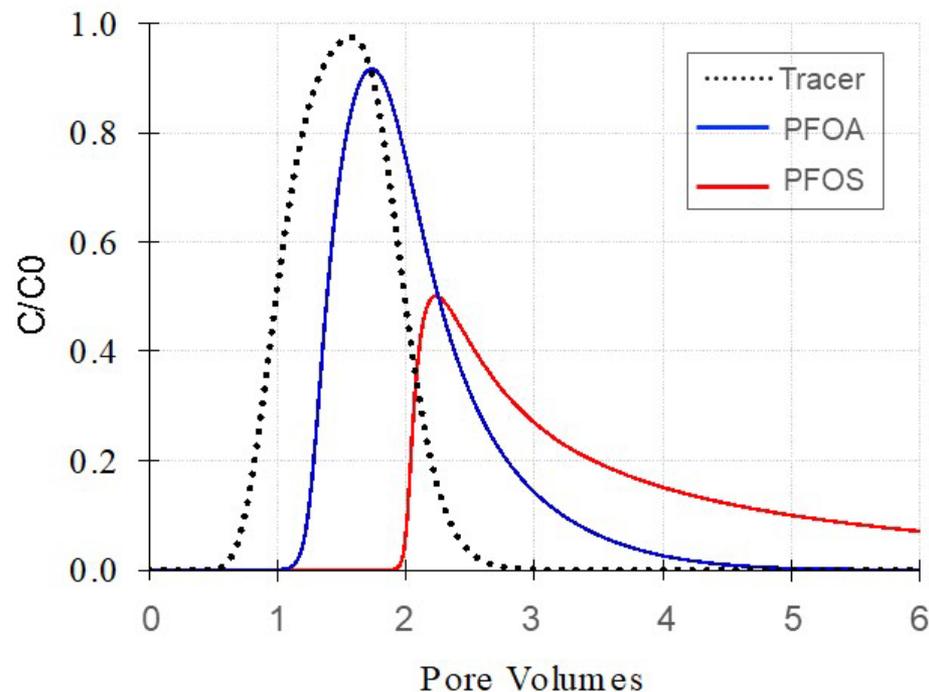
Specific Interfacial Area  $[L^{-1}]$ , 
$$A_{ai} = SA \left( 0.9031 - 0.9012 \frac{\theta}{\theta_s} \right)$$

SA: Geometric surface area  $[L^{-1}] = \frac{6(1 - \phi)}{d_{50}}$  (Costanza-Robinson et al., 2008)

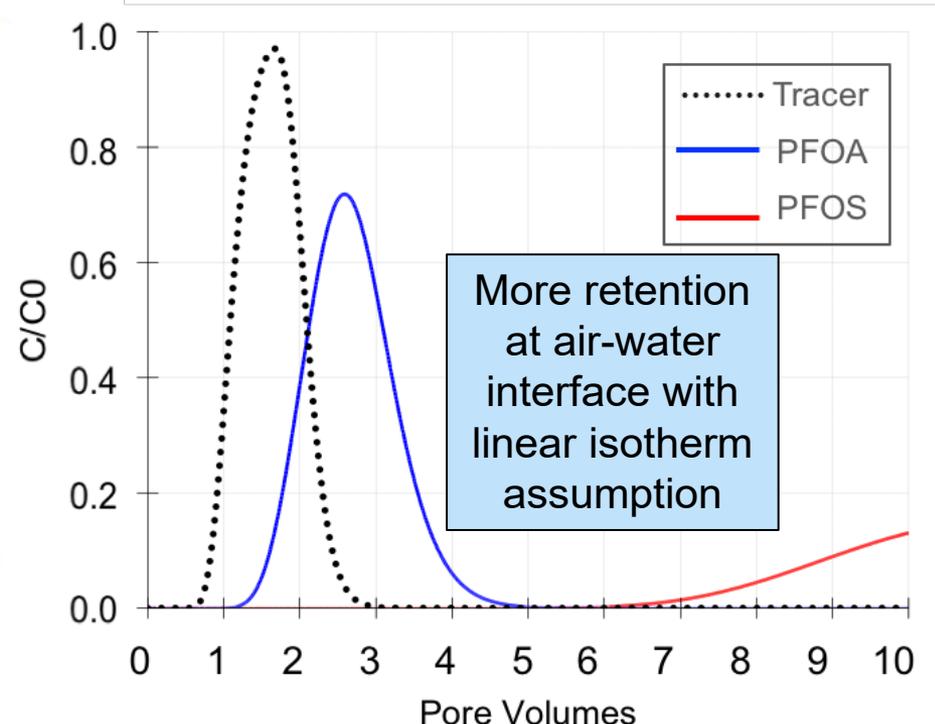
$\theta_w$ : water content,  $\theta_s$ : saturated water content,  $\phi$ : porosity,  $s_{\alpha}$ : saturation of  $\alpha$  - phase

# Effect of PFAS Accumulation at Air-Water Interface on Unsaturated Zone Transport

## Langmuir/Szyszkowski Isotherm



## Linear Partitioning

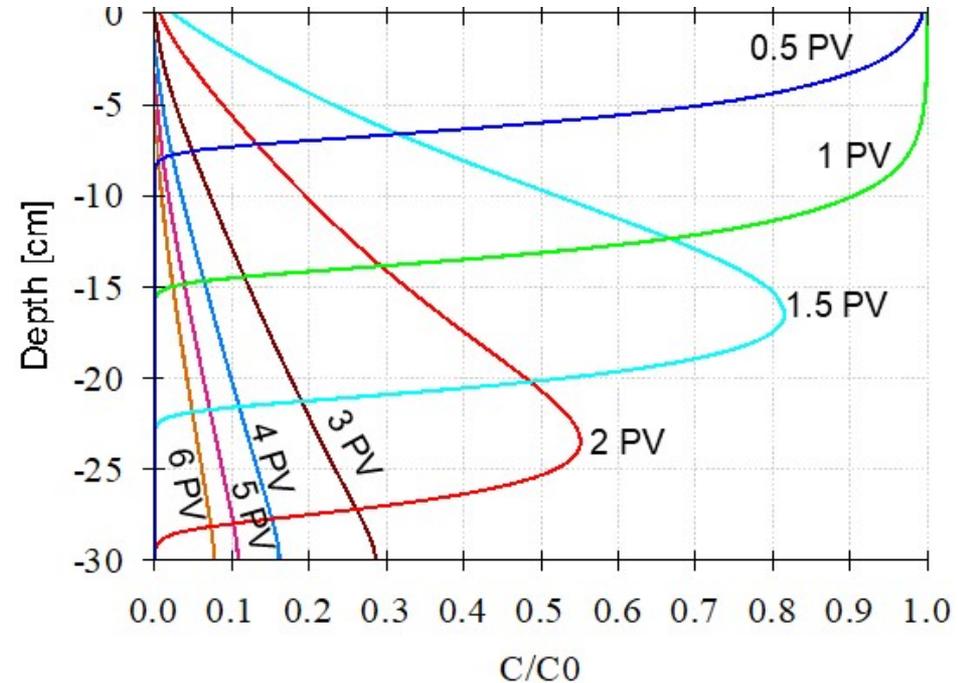
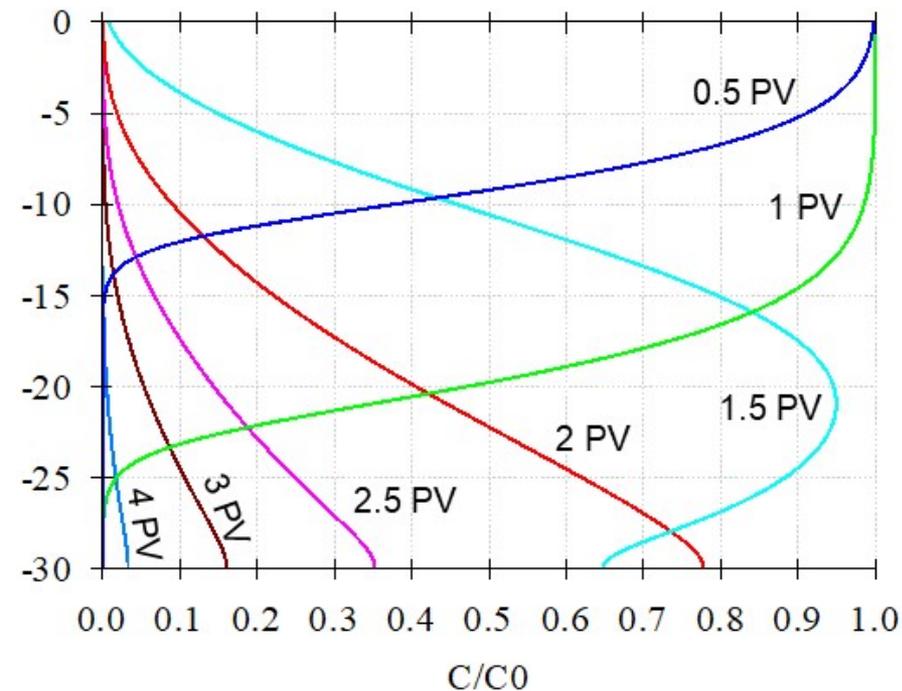


- Pulse injection (1 PV) of PFOA or PFOS (10 mg/L)
- Medium level of total dissolved solids (400 mg/L TDS)
- F-70 Ottawa sand (40-270 mesh)
- Uniform water content,  $\theta_w = 0.27$

# PFAS Vertical Concentration Profiles in Unsaturated Soil

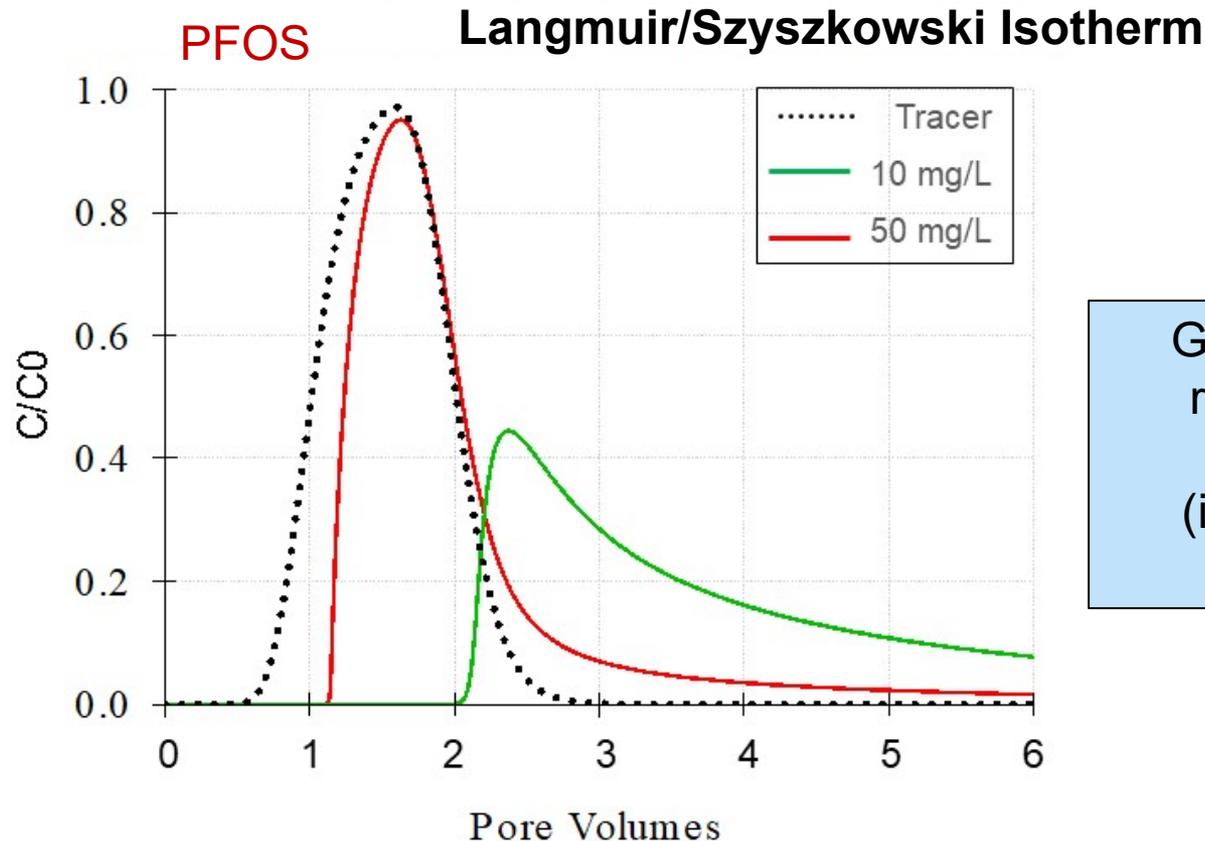
PFOA

Langmuir/Szyszkowski Isotherm



- Pulse injection (1 PV) of PFOA or PFOS (10 mg/L)
- Medium level of total dissolved solids (400 mg/L TDS)
- F-70 Ottawa sand (40-270 mesh)
- Uniform water content,  $\theta_w = 0.27$

# Effect of Input Concentration on Unsaturated Zone Transport of PFOS



Greater proportion retained at lower concentrations (influence of non-linearity)

- Pulse injection (1 PV) of PFOS (10 mg/L or 50 mg/L)
- Medium level of total dissolved solids (400 mg/L TDS)
- F-70 Ottawa sand (40-270 mesh)
- Uniform water content,  $\theta_w = 0.27$

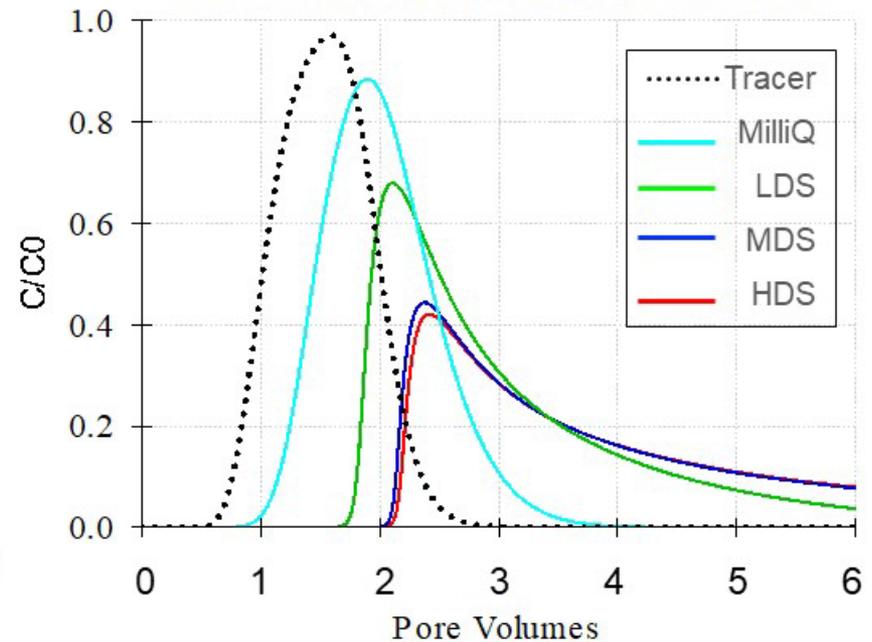
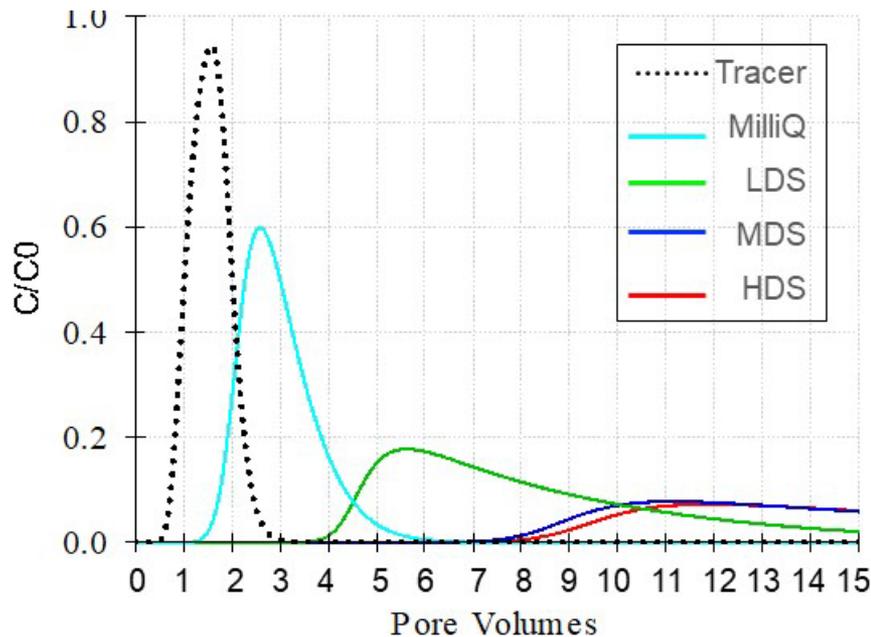
# Effect of Soil Water Content and TDS on PFOS Transport

$$\text{Interfacial Area [L}^{-1}\text{]}, A_{ai} = SA \left( 0.9031 - 0.9012 \frac{\theta_w}{\theta_s} \right)$$

$\theta_w = 0.20$

Langmuir/Szyszkowski Isotherm

$\theta_w = 0.27$



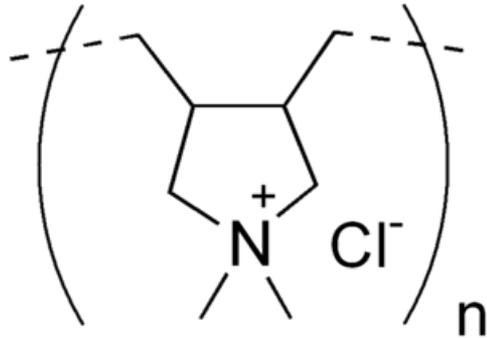
- Pulse injection (1 PV) of PFOS (10 mg/L)
- F-70 Ottawa sand (40-270 mesh)
- Uniform water content,  $\theta_w = 0.20$  or 27

# In Situ Sequestration of PFAS

# Coagulant polymers (cationic surfactants)

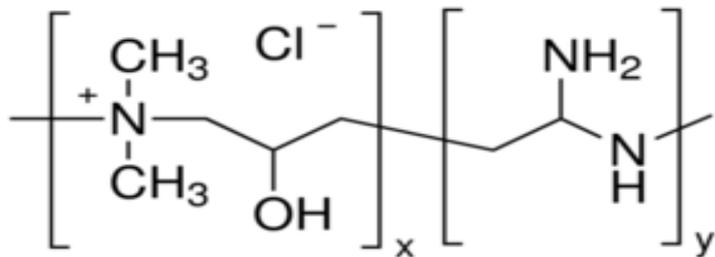
*SERDP Project ER-2425*

## Poly-DADMAC (PDM)



- Accepta 4351
- ~ 28% OC
- Quaternary Amine
- diallyl dimethylamine
- MW ~ 350,000

## Polyamine (PA)



- Accepta 4350
- ~ 26% OC
- Quaternary Amine
- epichlorohydrine and dimethylamine
- MW ~ 240,000



# To improve performance....combine Powdered Activated Carbon (PAC) with polyDADMAC (PDM)

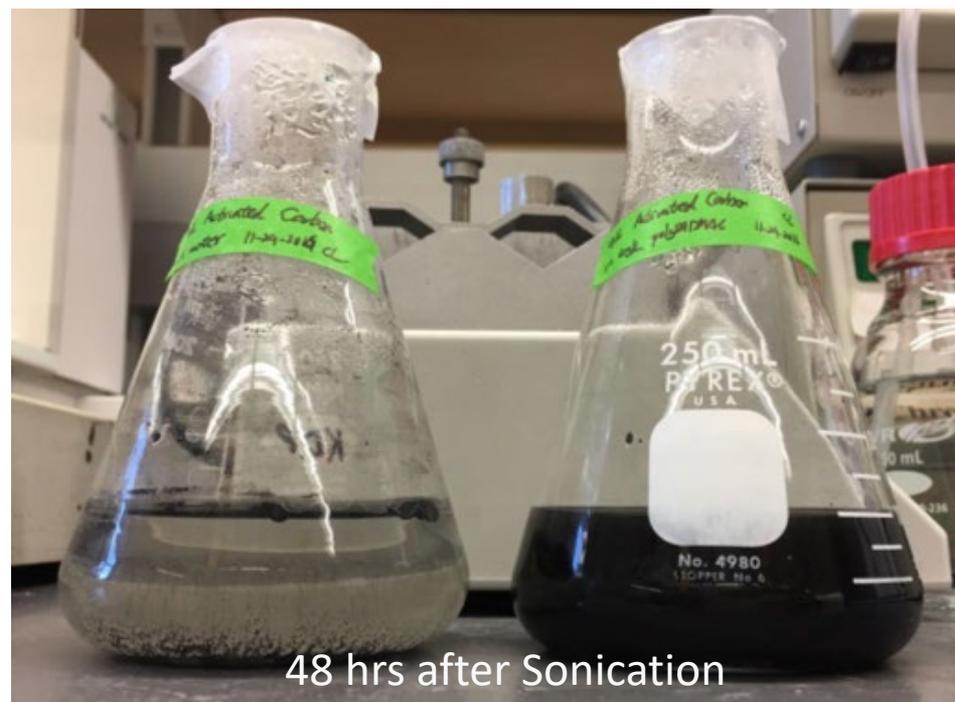
- ❖ PDM acts to stabilize PAC in suspension, facilitates delivery
- ❖ Both PDM and PAC can serve as sorbents (wide range of effectiveness)

1 g/L PAC

1 g/L PAC + 5 g/L PDM

1 g/L PAC

1 g/L PAC + 5 g/L PDM



DARCO® 100 mesh (150  $\mu$ m)

Powdered Activated Carbon (Sigma Aldrich)

Provisional Patent Application: Reg. No. 41,942, Docket No. 70011-067P01v (September, 2017)

# Commercially Available (Proprietary) PFAS Sorbents



## RemBind™-Tersus

Activated carbon, aluminum hydroxide, organic matter and other additives, intended for near surface soil mixing

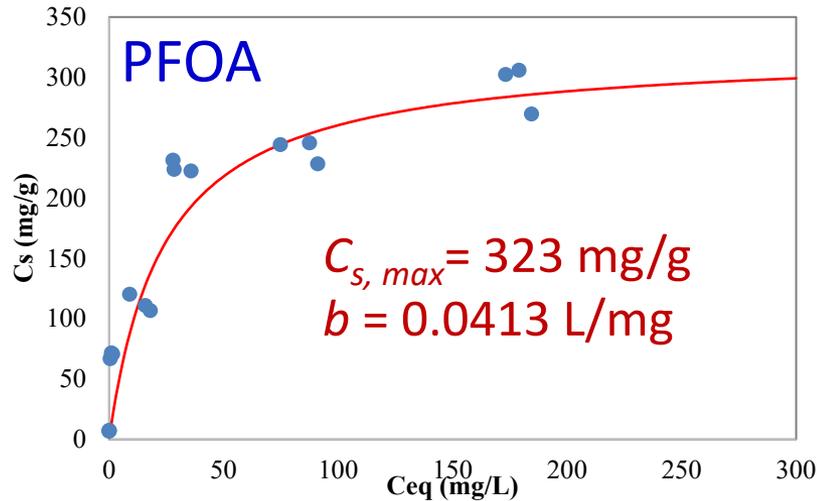


## PlumeStop® Liquid Activated Carbon™-Regenesis

Activated carbon (1-2 $\mu$ m) suspended in water dispersed with organic polymer

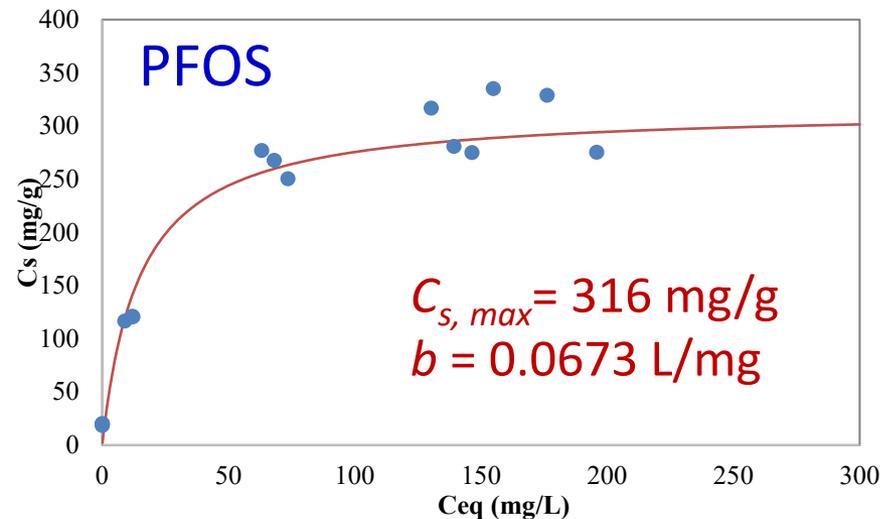
- ❖ Limited independent verification
- ❖ Limited data (e.g., mass balance)
- ❖ In situ delivery issues rarely addressed

# PFOA and PFOS Batch Adsorption Studies With Darco<sup>®</sup> PAC (100-mesh)

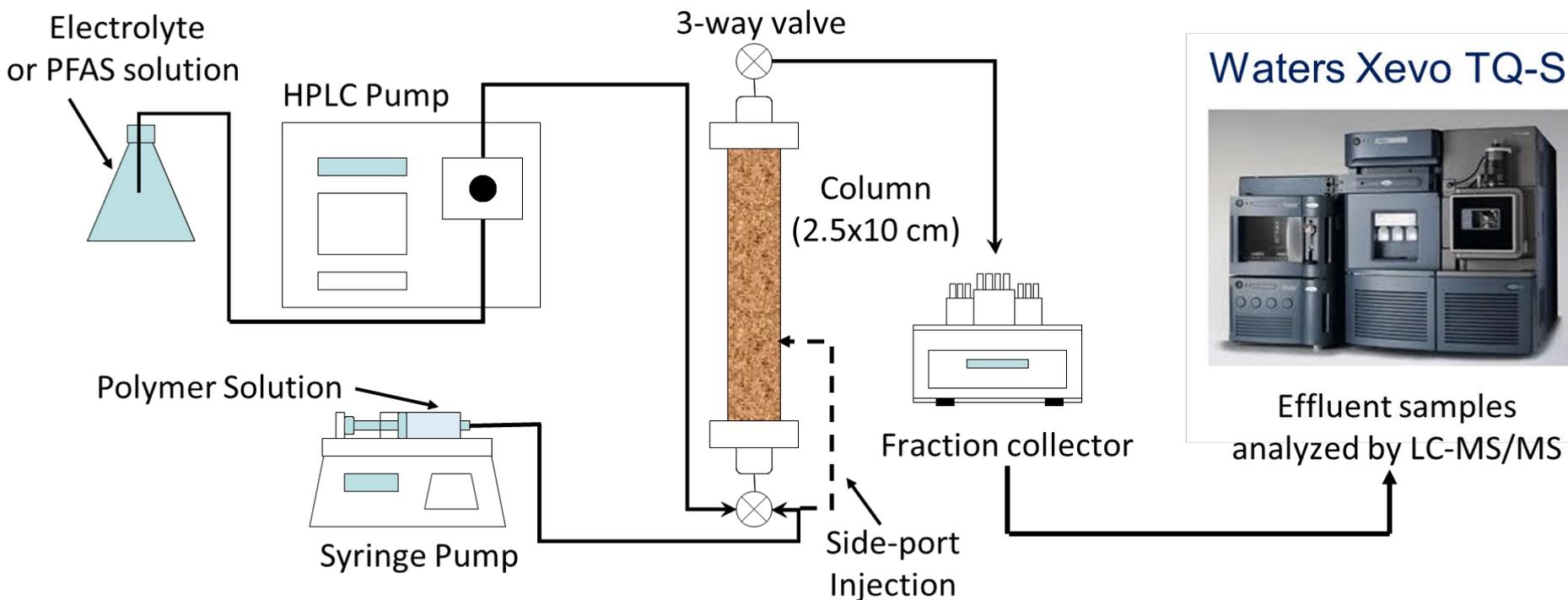


Langmuir Isotherm

$$C_s = \frac{C_{s, max} * b * C_{w, eq}}{1 + b * C_{w, eq}}$$



# Schematic Diagram of 1-D Column System



- (1) Non-reactive tracer test (pulse injection),
- (2) Inject PDM+PAC suspension,
- (3) Inject background electrolyte,
- (4) Inject PFAS solution (e.g., 100 ug/L PFOS)

# Injection of PDM+PAC Suspension

t = 0  
PV



after 3.5 PV  
PAC+PDM



after 3.5 PV  
background



26.8 mg of  
PAC retained  
in column

Flow  
Direction



40-50 mesh Ottawa Sand ( $d_{50} = 358 \mu\text{m}$ ),  $k_i = 7.37 \times 10^{-11} \text{ m}^2$ ,  $n = 0.37$ ,  $\text{SSA} = 0.0125 \text{ m}^2/\text{g}$ ,  
PV = 22 mL

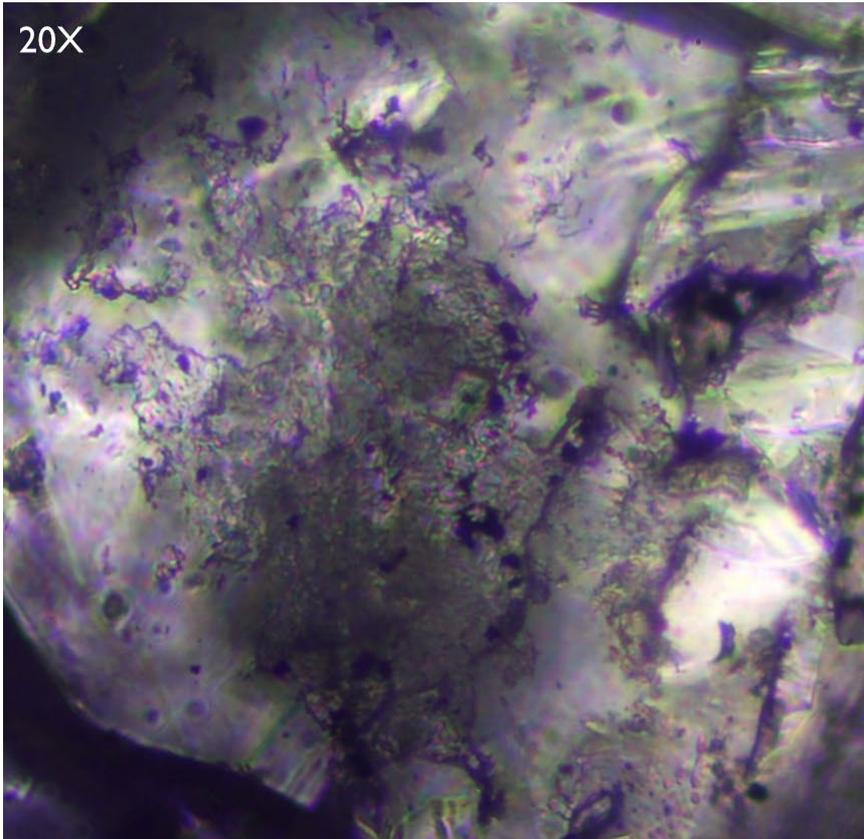
PDM+PAC Suspension: 1,000 mg/L PAC + 5,000 mg/L PDM, viscosity = 1.18 cP

Flow rate: 0.12 mL/min; pore-water velocity  $\sim 1.0 \text{ m/day}$

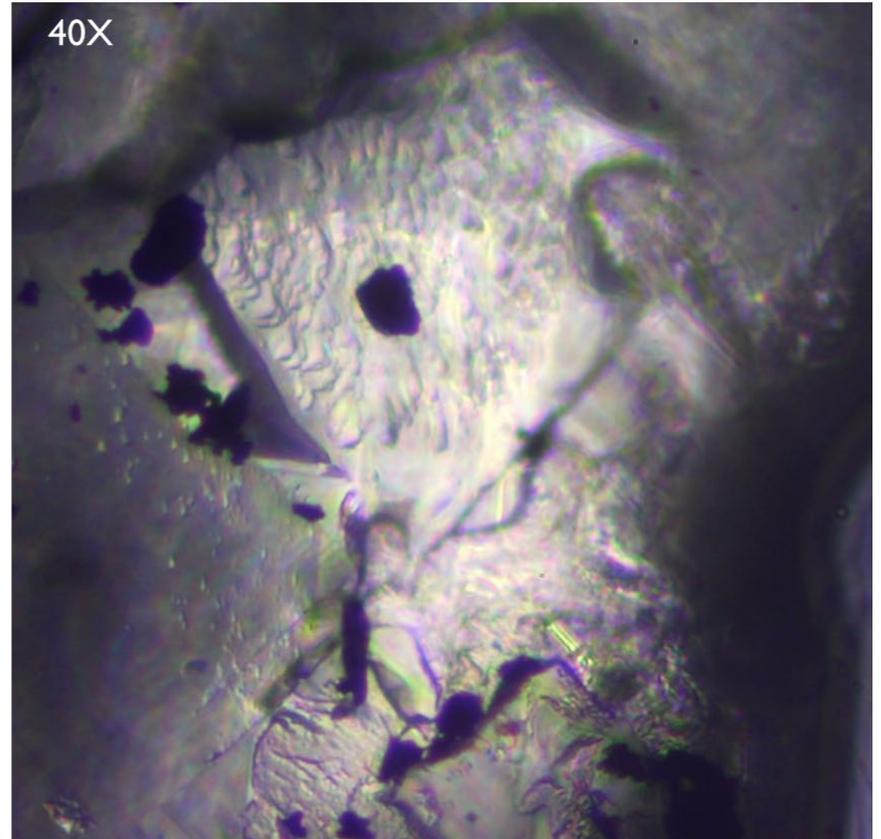
# Images of PDM+PAC Treated Ottawa Sand

Leica DM IL LED

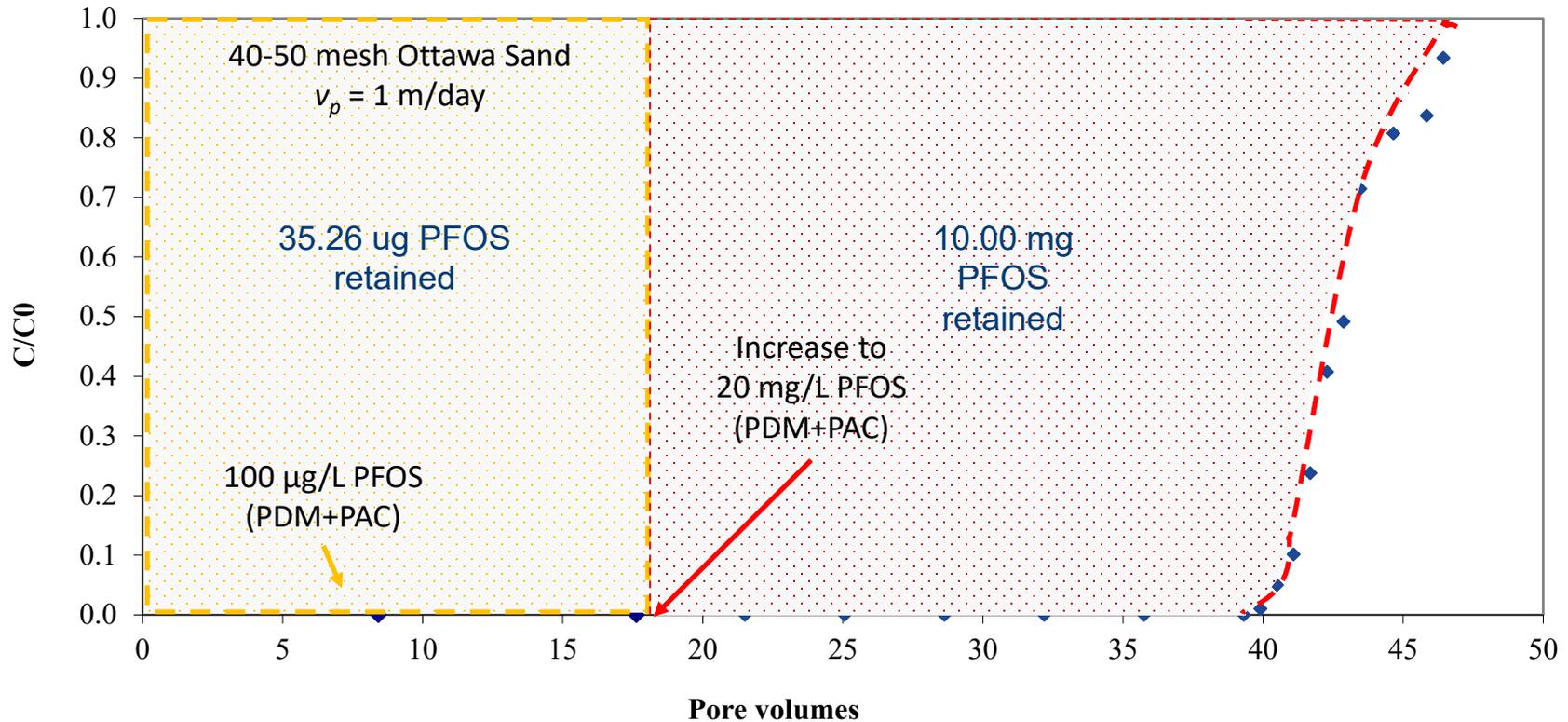
20X



40X



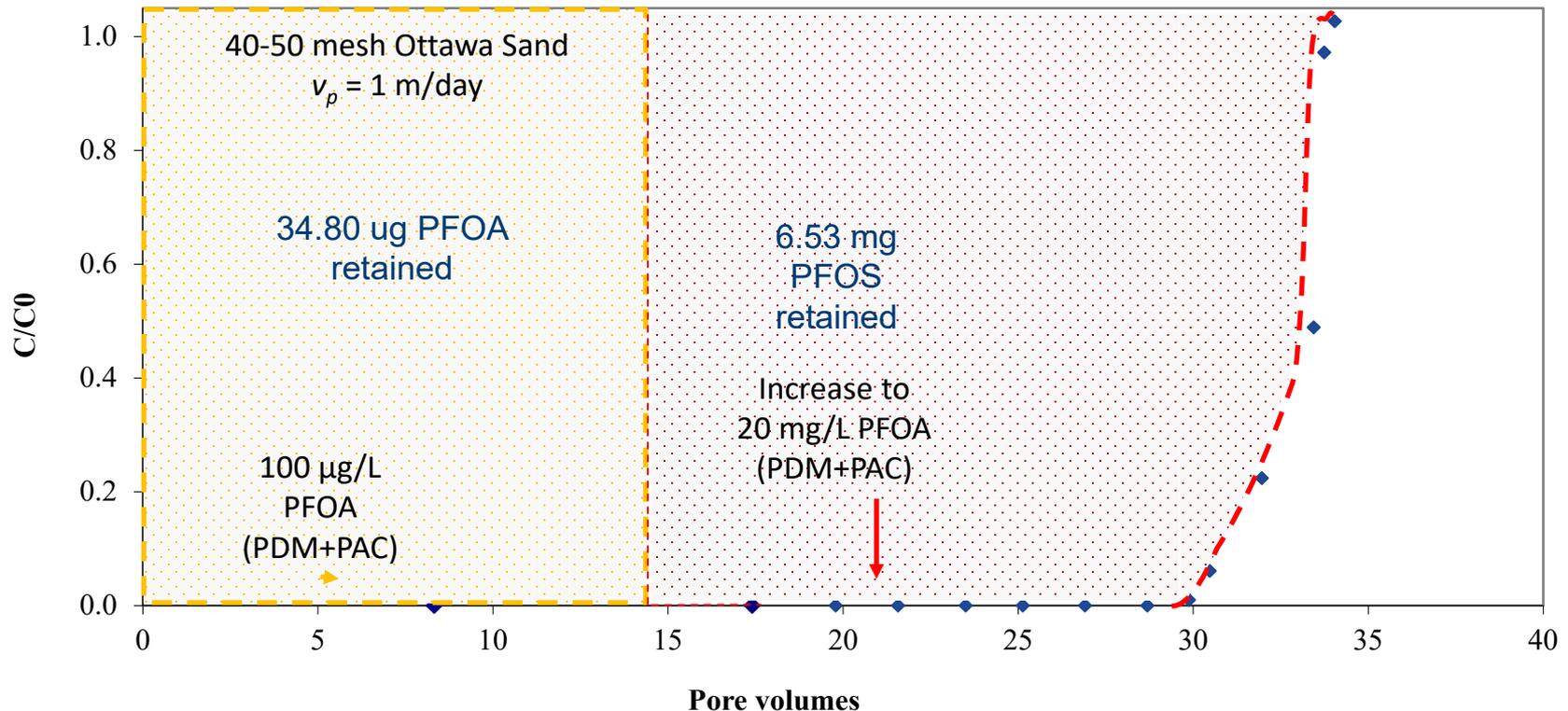
# PFOS Column: S-PAC treated 40-50 mesh Ottawa Sand



Based on the measured  $C_{s,max} = 316$  mg/g and mass of retained PAC (~27 mg), the capacity of the column should be ~ 8.65 mg PFOS, consistent with the observed retention of ~10.04 mg PFOS

For a 100 µg/L injection; ~2 µg PFOS retained/PV, capacity would be reached after ~5,020 PV

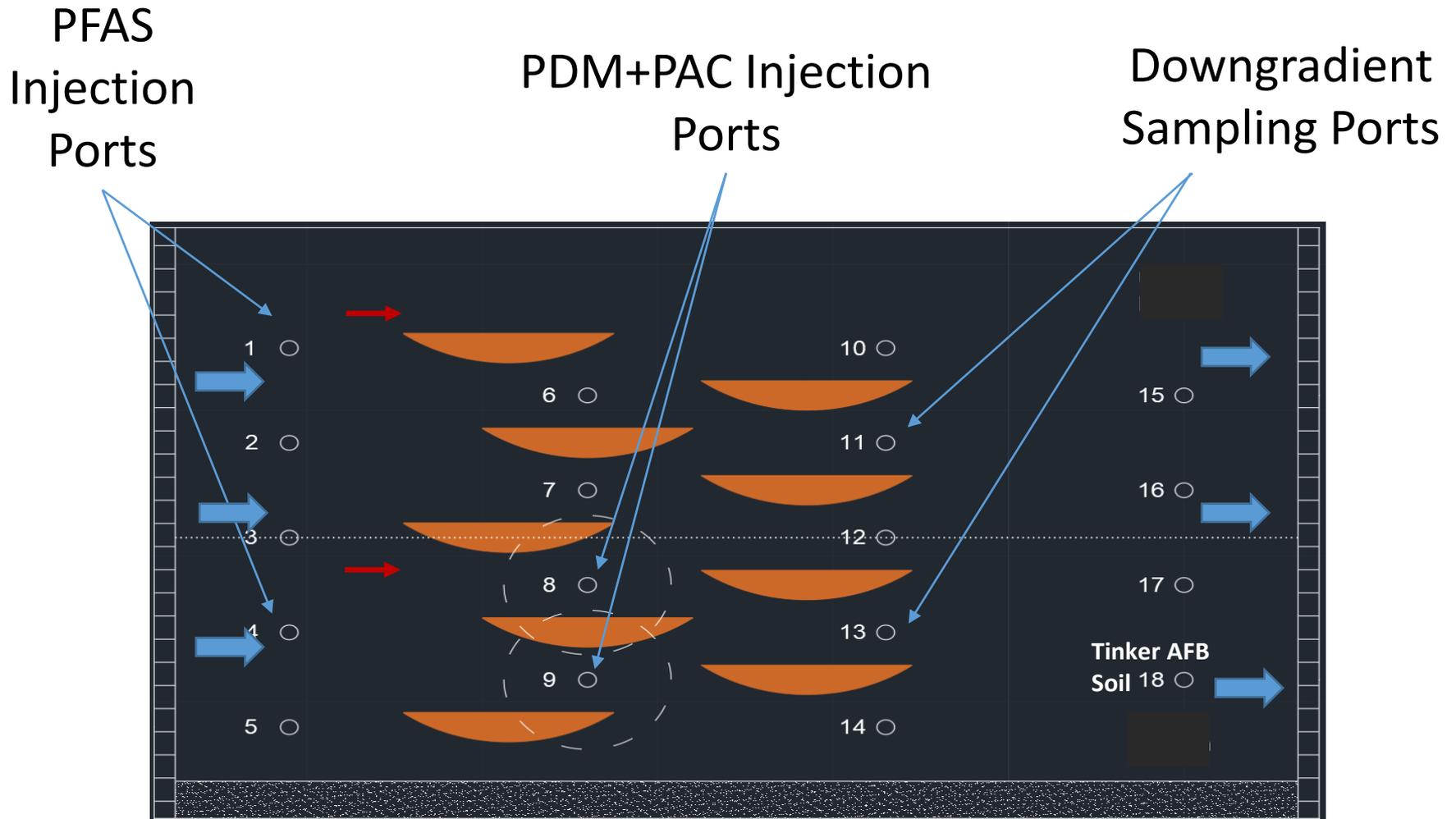
# PFOA Column: S-PAC treated 40-50 mesh Ottawa Sand



Based on the measured  $C_{s,max} = 323$  mg/g and mass of retained PAC (~14.8 mg), the capacity of the column should be ~ 4.78 mg PFOS, consistent with the observed retention of ~6.57 mg PFOA

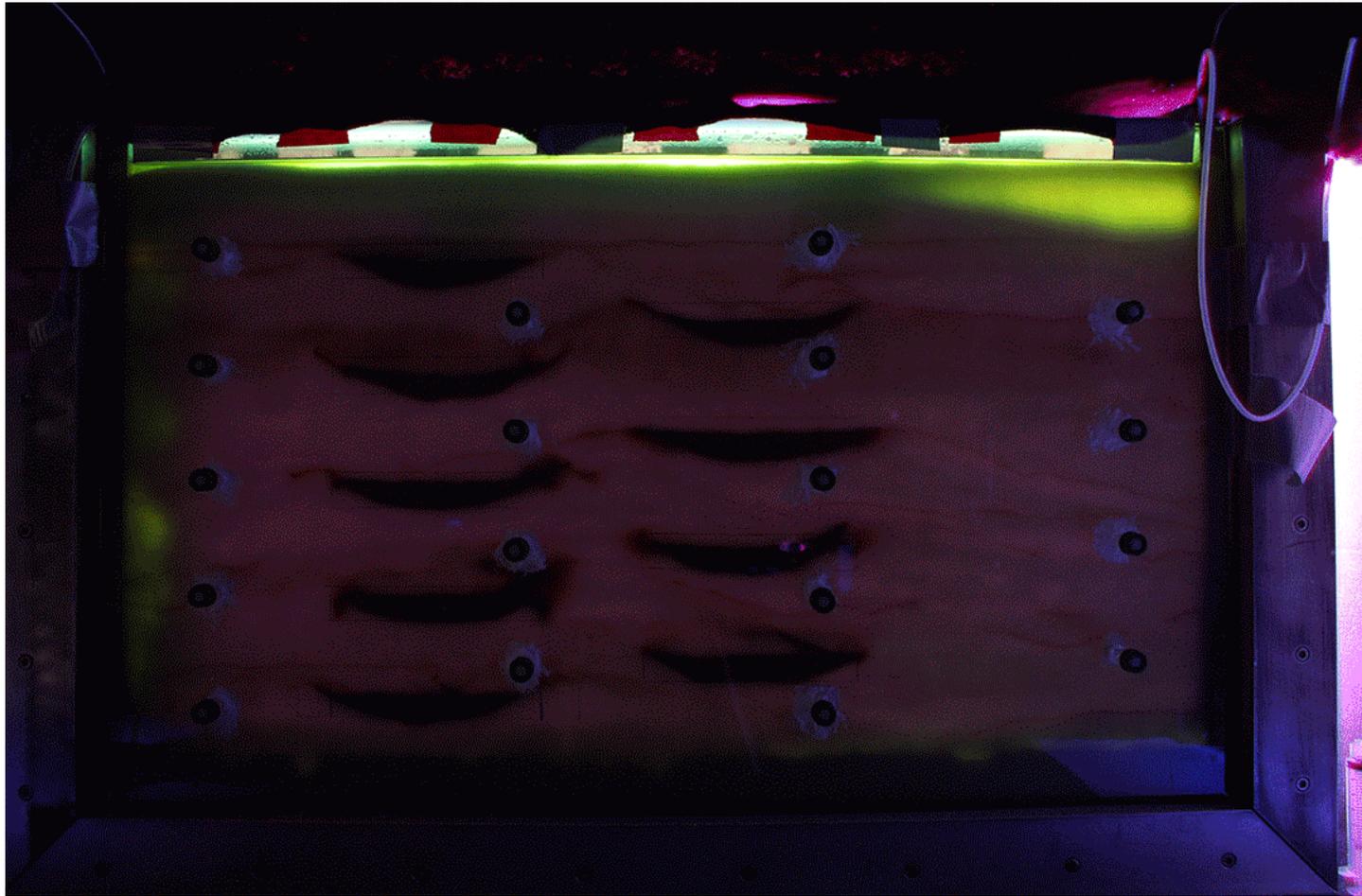
For a 100  $\mu$ g/L injection; ~2 ug PFOA retained/PV, capacity would be reached after ~3,600 PV

# Configuration of Aquifer Flow Cell



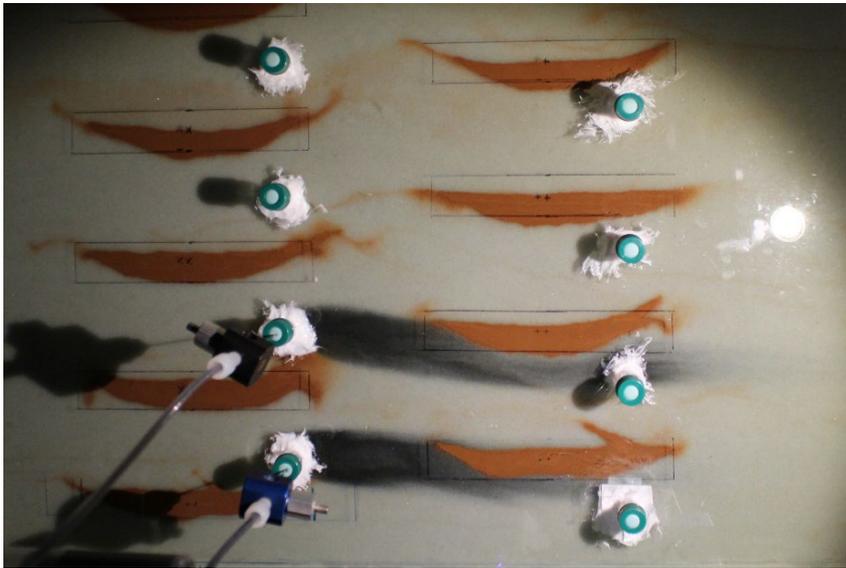
PV=1.45L

# Tracer Test Before PDM+PAC Injection

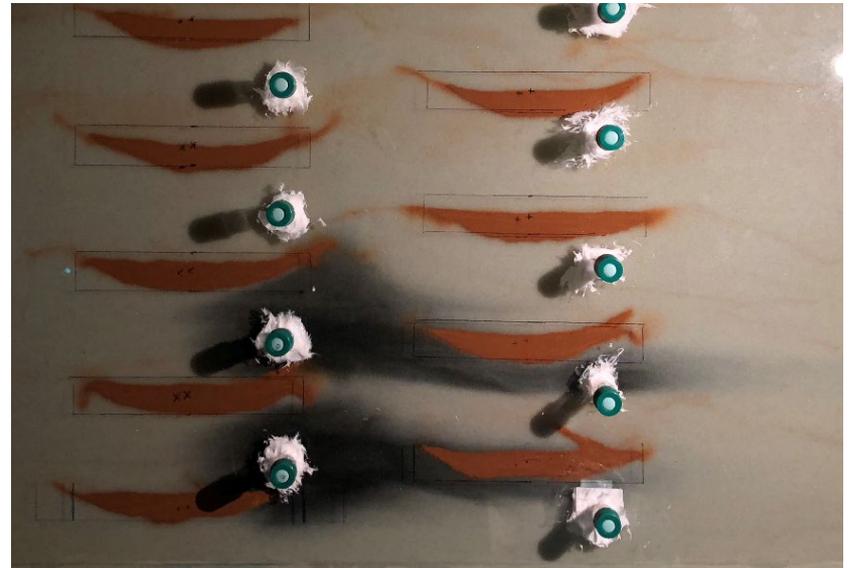


# Side-port Injection of 1 g/L PAC + 5 g/L PDM

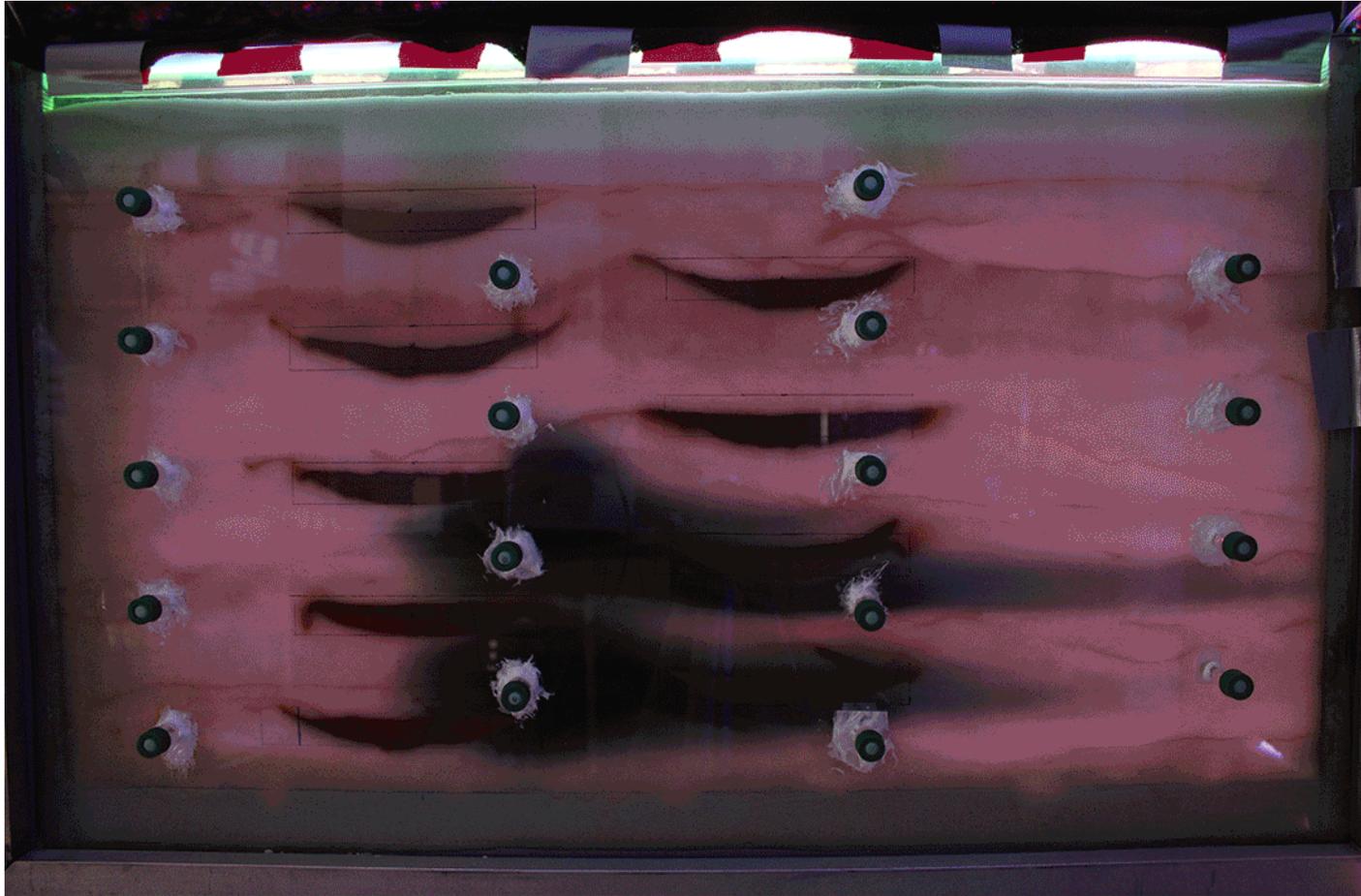
40 mL (0.08 mL/min) with  
background flow (2.4 mL/min)



80 mL (0.08 mL/min) with no  
background flow



## Tracer Test After PDM+PAC Injection



# Acknowledgements



Projects ER-2425 and  
ER18-1149



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UNIVERSITY

School of  
Engineering



UNIVERSITY OF MINNESOTA

**JACOBS**